



# FUEL-SWITCHING HYDRONIC SYSTEMS USING AIR-TO-WATER HEAT PUMPS

**ASHRAE WINNIPEG CHAPTER  
TECHNICAL PRESENTATION, MARCH 16, 2023**

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# TOPICS

- **AIR-TO-WATER HEAT PUMP RECAP**
  - TECHNOLOGY OVERVIEW & DESIGN CONSTRAINTS & SIZING METHODOLOGIES
- **FUEL-SWITCHING HYDRONIC SYSTEMS**
  - ENERGY & GHG EMISSION SAVINGS COMPARISON:
    - ALL-ELECTRIC SYSTEMS VS. BACK-UP NATURAL GAS
    - COST COMPARISON: NATURAL GAS VS. ELECTRIC
- **CENTRAL AIR-TO-WATER HEAT PUMP PLANT SIZING & APPLICATIONS**
  - 2-PIPE CHANGEOVER SYSTEMS
  - HEAT PUMP CASCADE SYSTEMS (2-PIPE)
  - HYBRID 4-PIPE CENTRAL PLANT
  - HEAT RECOVERY
  - HIGH-TEMPERATURE RETROFITS

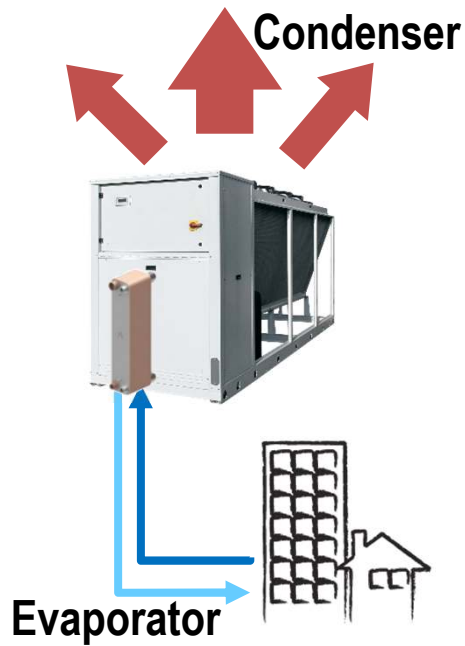
# LEARNING OBJECTIVES

- **Understand the concept of fuel-switching and its importance for high efficiency retrofit of existing building central plant systems.**
- **Learn design strategies and application techniques of using air-to-water heat pump plant equipment.**
- **Learn about the energy and cost savings, and emission reductions achievable with fuel-switching retrofit of traditional central plant systems with air-to-water heat pumps**

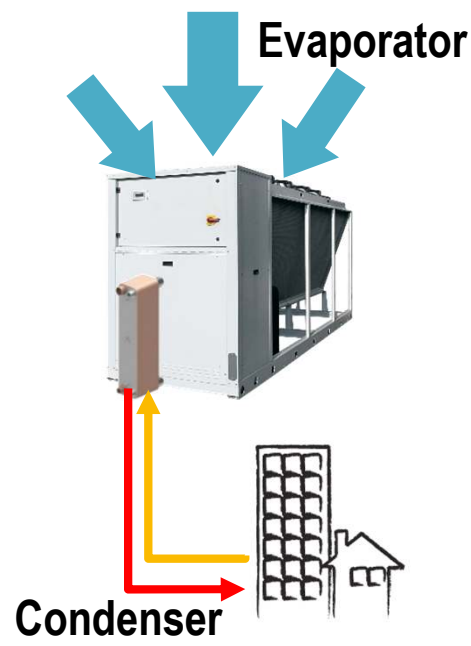


# REVERSIBLE AIR-TO-WATER HEAT PUMP: OPERATING PRINCIPLE

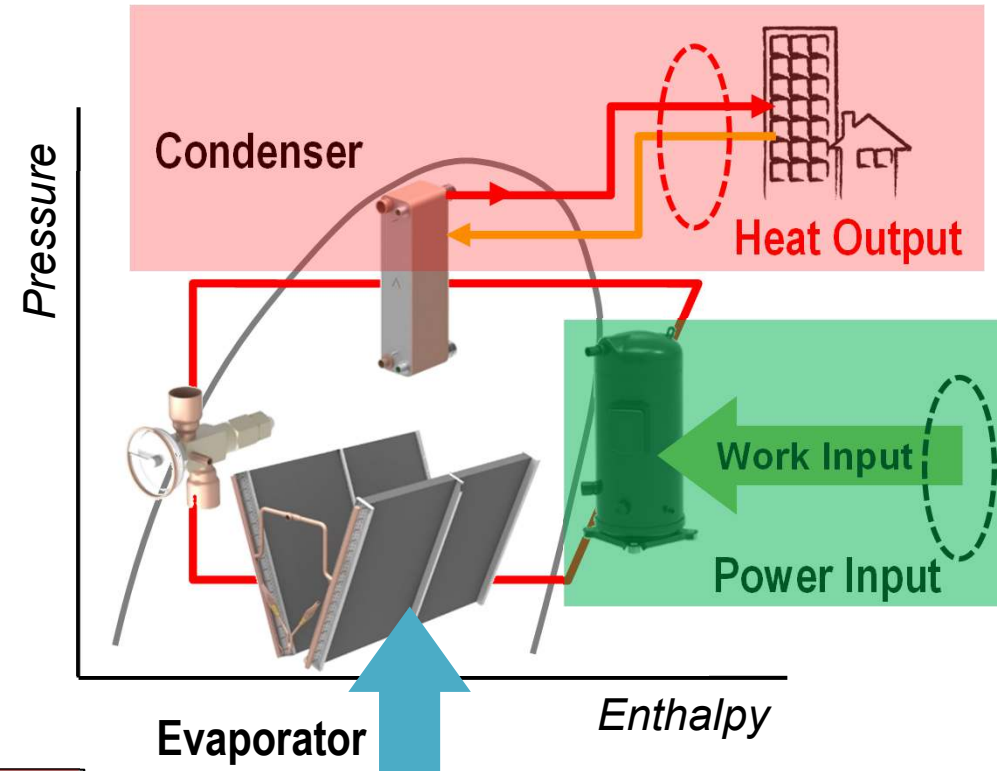
## COOLING MODE



## HEATING MODE



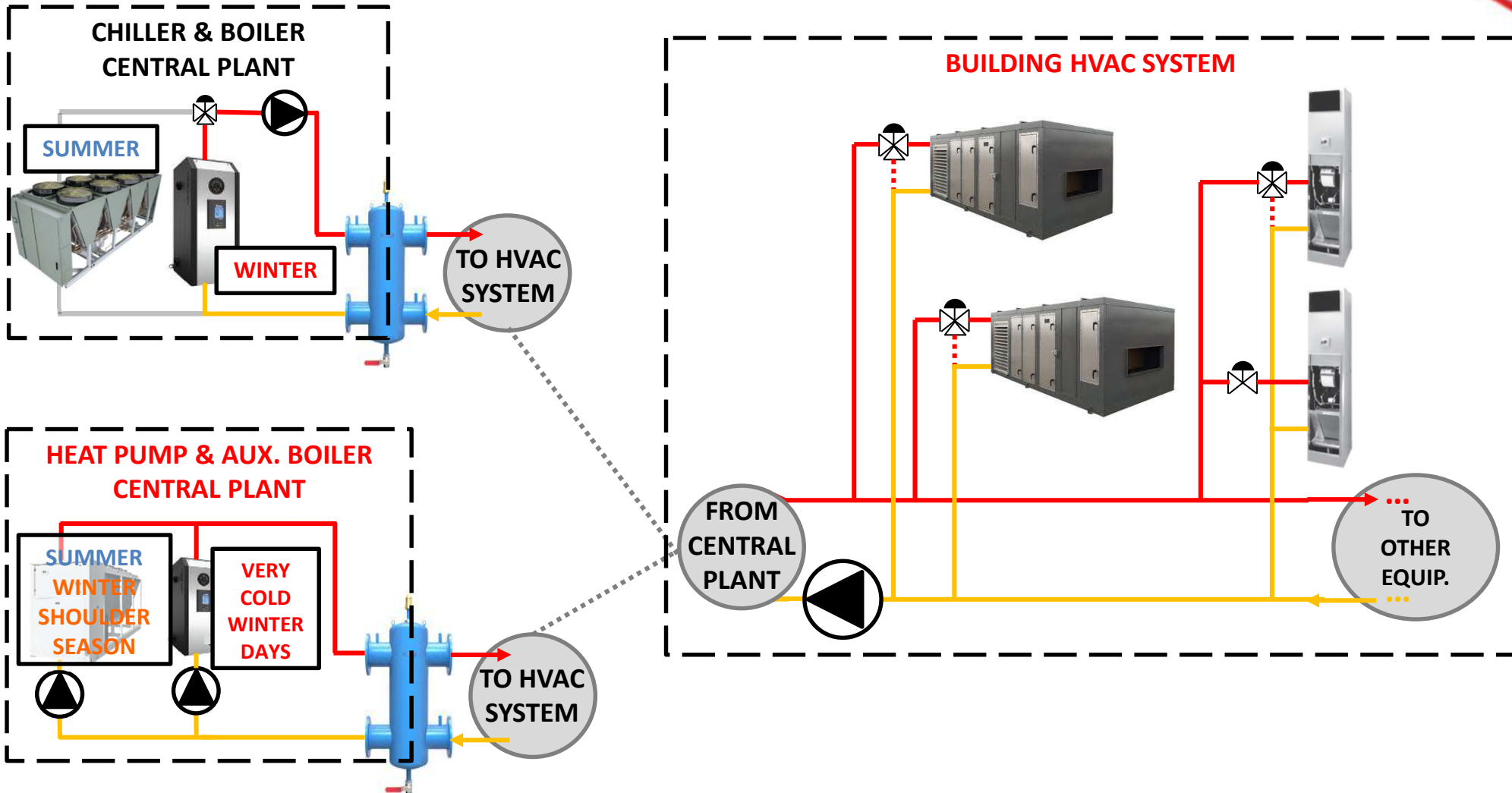
## VAPOR-COMPRESSION REFRIGERATION CYCLE (HEATING MODE)



Coefficient of Performance:

$$COP = \frac{\text{Heat Output } \left( \frac{BTU}{h} \text{ or Watts} \right)}{\text{Power Input (Watts)}}$$

# CENTRAL HYBRID HEAT PUMP PLANT

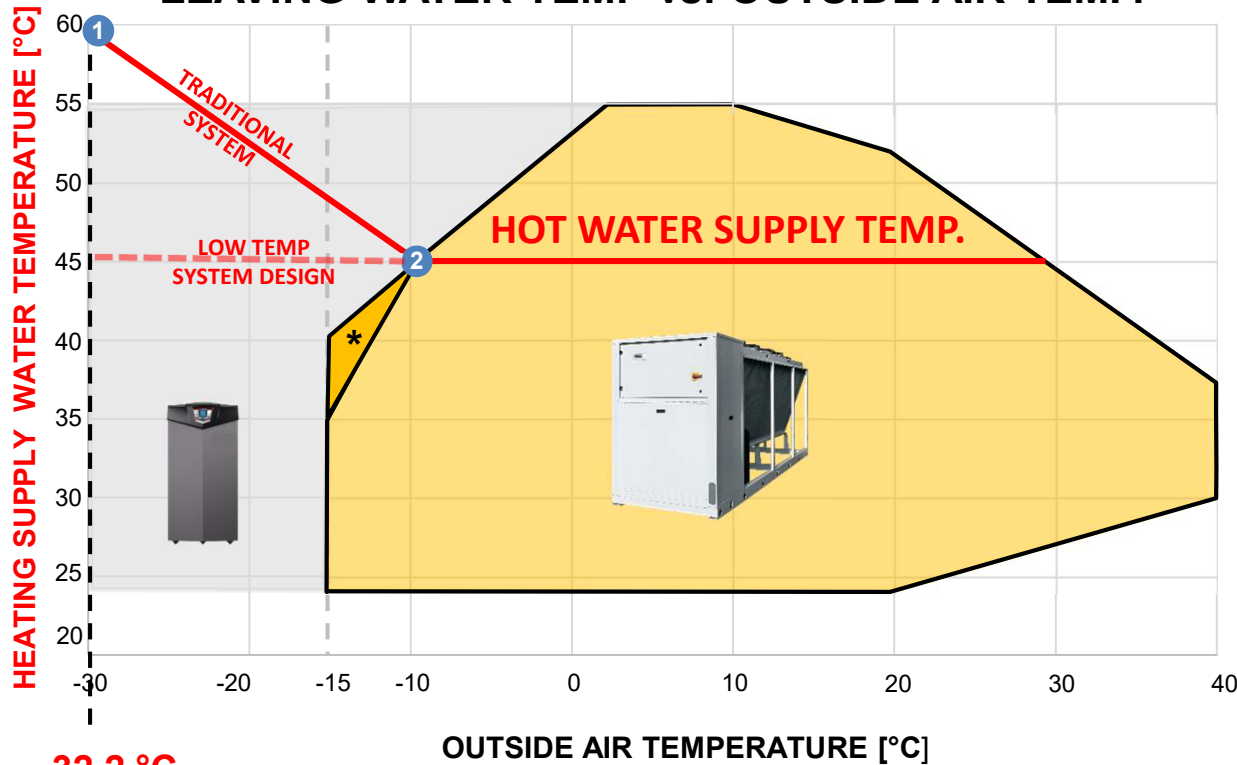


# AIR-TO-WATER HEAT PUMP: DESIGN CONSIDERATIONS

- UNDERSTAND THE INFLUENCE OF OUTSIDE AIR TEMPERATURE
- DESIGN HYDRONIC SYSTEM BASED ON HEAT PUMP CAPABILITIES INSTEAD OF FITTING INTO EXISTING DESIGN PRACTICES
- **HEAT PUMP PERFORMANCE VARIES WITH OUTSIDE AIR TEMPERATURE:**
  1. **SUPPLY TEMPERATURE REDUCTION (OPERATING ENVELOPE)**
  2. **CAPACITY REDUCTION**
  3. **COEFFICIENT OF PERFORMANCE REDUCTION**

# AIR-TO-WATER HEAT PUMP: OPERATING ENVELOPE

## FULL LOAD HEATING OPERATING LIMITS LEAVING WATER TEMP vs. OUTSIDE AIR TEMP.



**-32.2 °C**

**Winnipeg Int'l Airport Winter Design Temp (ASHRAE 99.6%D.B.)  
(ASHRAE 99% D.B. = -29.9 °C)**

## APPLICATION CONSIDERATIONS:

- Select **LOWEST DESIGN SUPPLY TEMPERATURE** Feasible
- Consider **HIGHER BOILER SUPPLY WATER TEMPERATURE** below ASHP cut-out
- Can the Heat Pump meet the **HEATING LOAD** using a Lower Supply Temp. at Milder Conditions?

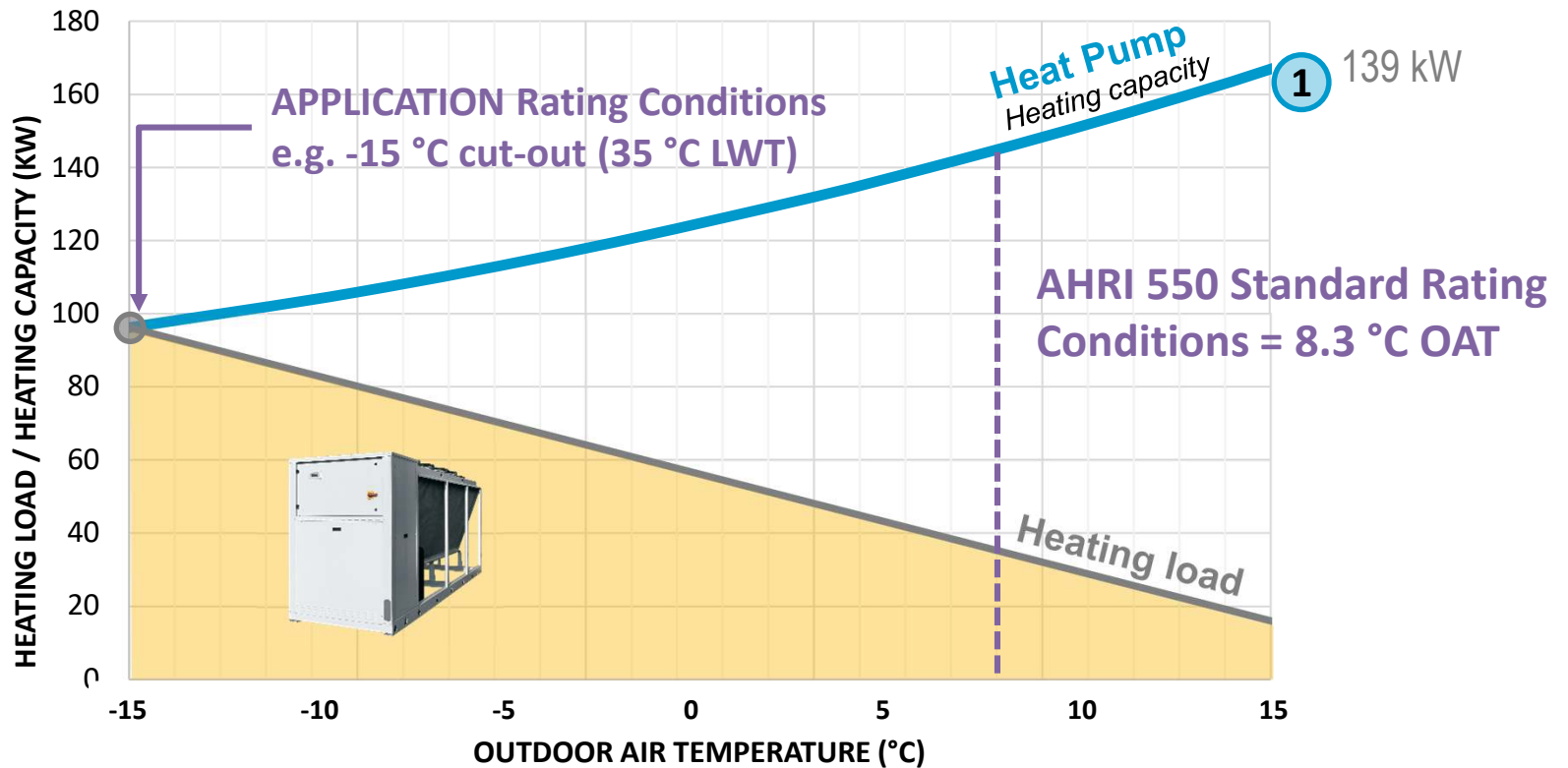
# AIR-TO-WATER HEAT PUMP: SIZING FOR HEATING

## HEATING CAPACITY VS HEATING LOAD

138 kW ATW HP (NOMINAL)



REVERSIBLE UNIT, AIR SOURCE FOR OUTDOOR INSTALLATION



Heat Pump

100%



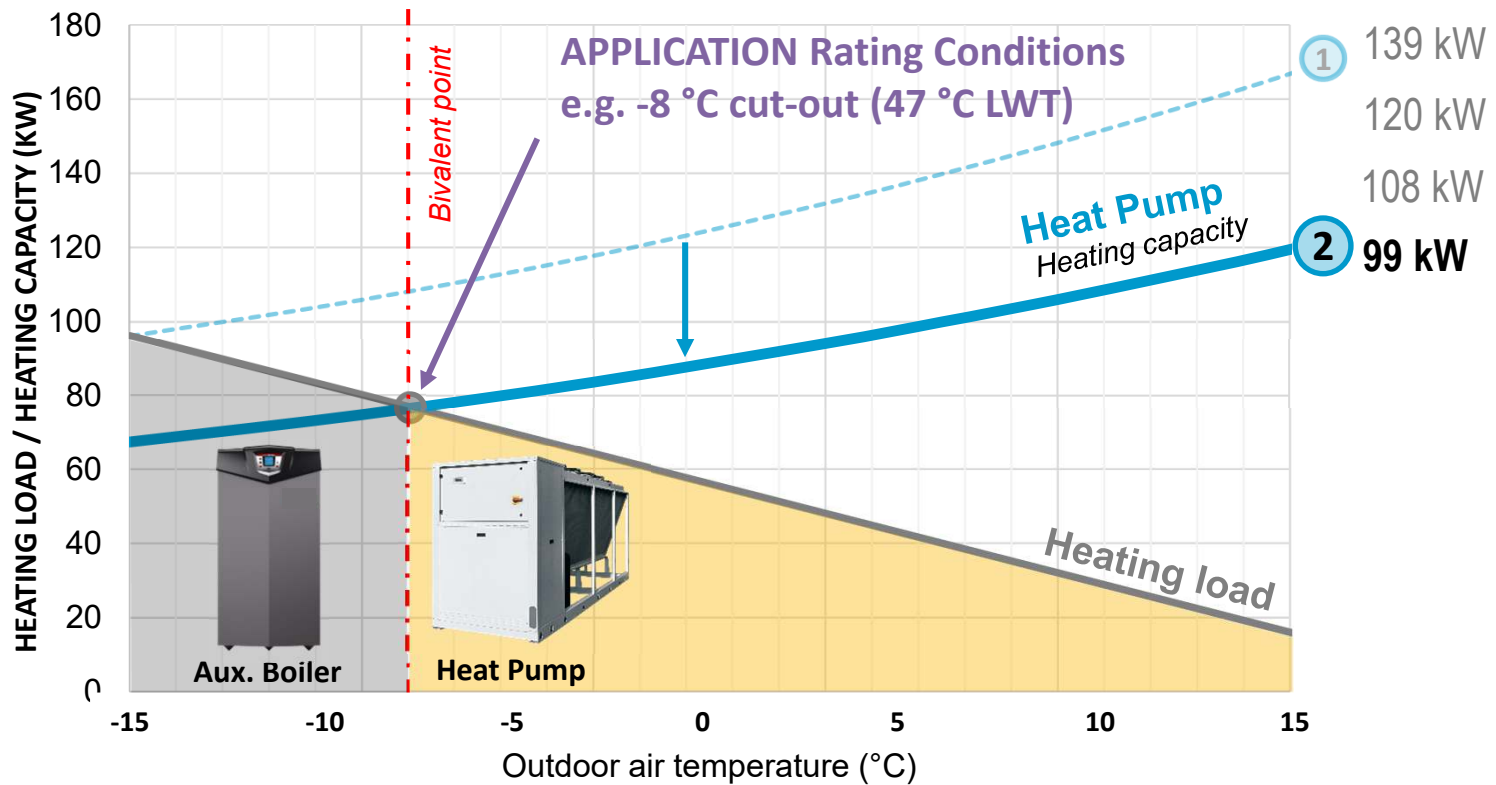
# AIR-TO-WATER HEAT PUMP: SIZING FOR HEATING

## HEATING CAPACITY VS HEATING LOAD

99 kW ATW HP (NOMINAL)



REVERSIBLE UNIT, AIR SOURCE FOR OUTDOOR INSTALLATION



- ① 139 kW
- 120 kW
- 108 kW
- ② 99 kW

Auxiliary

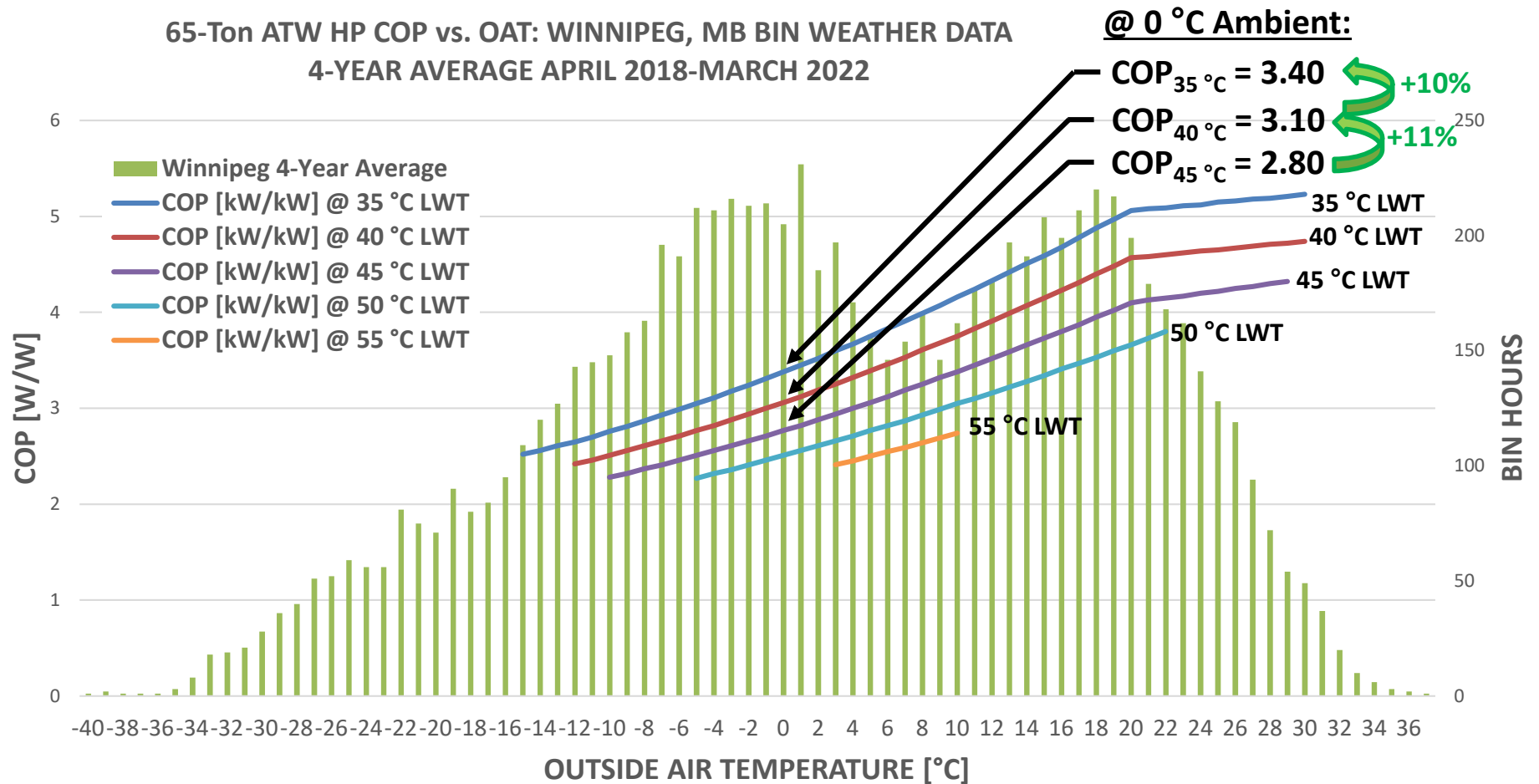
Heat Pump

PRICE

FOOTPRINT

# INFLUENCE OF OUTDOOR AIR TEMPERATURE: COP

## AIR-TO-WATER HEAT PUMP COP VS. OUTSIDE AIR TEMPERATURE & BIN HOURS



# BIN HOUR ANALYSIS FOR WINNIPEG, ON

## AUXILIARY BOILER USAGE HOURS BELOW CUT-OUT FOR VARIOUS SUPPLY WATER TEMPERATURE DESIGN SELECTION POINTS

### Med-High Temp Application

WINNIPEG, MB 4-YEAR AVERAGE BIN WEATHER DATA APRIL 2019 - APRIL 2022		
Temperature Range	4-YEAR AVERAGE ANNUAL HOURS	4-YEAR AVERAGE % OF HOURS
T < -5 °C	2,529	28.9%
-5 °C ≤ T ≤ +10 °C	2,986	34.1%
10 °C < T < 20 °C	2,000	22.8%
20 °C ≤ T	1,245	14.2%

### Med Temp Application

WINNIPEG, MB 4-YEAR AVERAGE BIN WEATHER DATA APRIL 2019 - APRIL 2022		
Temperature Range	4-YEAR AVERAGE ANNUAL HOURS	4-YEAR AVERAGE % OF HOURS
T < -10 °C	1,673	19.1%
-10 °C ≤ T ≤ +10 °C	3,842	43.9%
10 °C < T < 20 °C	2,000	22.8%
20 °C ≤ T	1,245	14.2%

### Low Temp Application

WINNIPEG, MB 4-YEAR AVERAGE BIN WEATHER DATA APRIL 2019 - APRIL 2022		
Temperature Range	4-YEAR AVERAGE ANNUAL HOURS	4-YEAR AVERAGE % OF HOURS
T < -15 °C	1,029	11.7%
-15 °C ≤ T ≤ +10 °C	4,486	51.2%
10 °C < T < 20 °C	2,000	22.8%
20 °C ≤ T	1,245	14.2%

Total Hours Below -5 °C: **2,529 Hours**  
~ 50 °C @ -5 °C Ambient

Total Hours Below -10 °C: **1,673 Hours**  
~ 45 °C @ -10 °C Ambient

Total Hours Below -15 °C: **1,029 Hours**  
~ 35 to 40 °C @ -15 °C Ambient

# CANADA GREEN BUILDING COUNCIL ZERO CARBON BUILDING DESIGN STANDARD v3 (JUNE 2022)

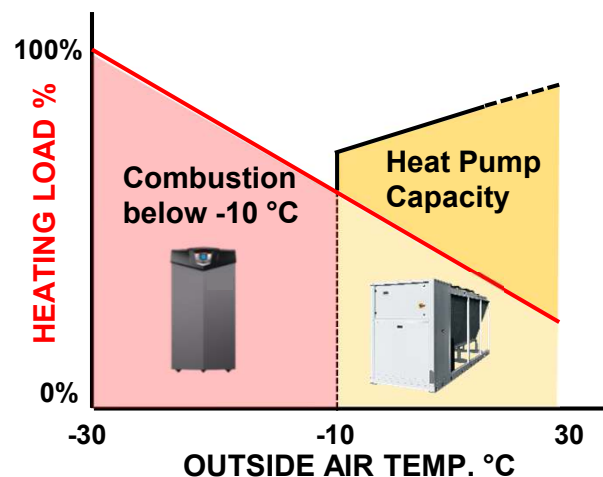
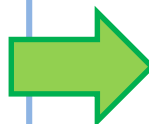
## REQUIREMENTS

### ONSITE COMBUSTION LIMIT FOR SPACE HEATING

Space heating systems should be designed to operate without onsite combustion whenever possible. However, to provide greater design flexibility and recognize current technological and financial barriers, some onsite combustion for space heating is permitted.

Projects must be capable of supplying all space heating with installed non-combustion-based technologies at an outdoor air temperature of  $-10\text{ }^{\circ}\text{C}$  or the design temperature, whichever is higher. Space heating technologies whose performance is not directly affected by outdoor air temperature (e.g., ground source heat pumps, electric resistance) must be demonstrated to be able to meet the same fraction of the annual heating demand as an air source heat pump system supported by onsite combustion. at outdoor air temperatures below  $-10\text{ }^{\circ}\text{C}$ .

**AUXILIARY COMBUSTION ACCEPTABLE  
PROVIDED THAT A ZERO CARBON TRANSITION  
PLAN ADDRESSES FUTURE ELIMINATION OF  
COMBUSTION BELOW  $-10^{\circ}\text{C}$  LIMIT**



SOURCE: CANADA GREEN BUILDING COUNCIL ZERO CARBON DESIGN STANDARD VERSION 3, PUBLISHED JUNE 2022. AVAILABLE: [CAGBC Zero Carbon Building-Design Standard v3.pdf](#)

# CANADA GREEN BUILDING COUNCIL ZERO CARBON BUILDING DESIGN STANDARD v3 (JUNE 2022)

## ZERO CARBON TRANSITION PLAN

ZCB-Design projects that use any onsite combustion for space heating or service hot water, regardless of whether zero emissions biofuels are used, must prepare a Zero Carbon Transition Plan. A Zero Carbon Transition Plan is a costed plan that outlines how a building will adapt over time to remove combustion from building operations. A well-crafted plan will leverage the natural intervention points in a building's capital plan, when retrofits would normally be required. ZCB-Design requires that the transition plan address space heating and service hot water.

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<sup>21</sup> See Section 3.1.3 of the report, available at, [www.cagbc.org/decarbonize](http://www.cagbc.org/decarbonize).

# HYBRID CENTRAL HEAT PUMP PLANT APPLICATIONS

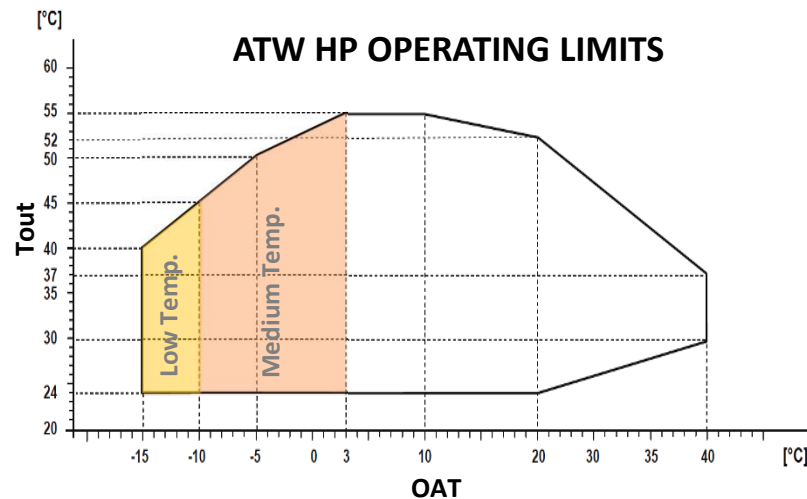
## AIR-TO-WATER HEAT PUMP APPLICATIONS:

### LOW TEMPERATURE HEATING APPLICATIONS:

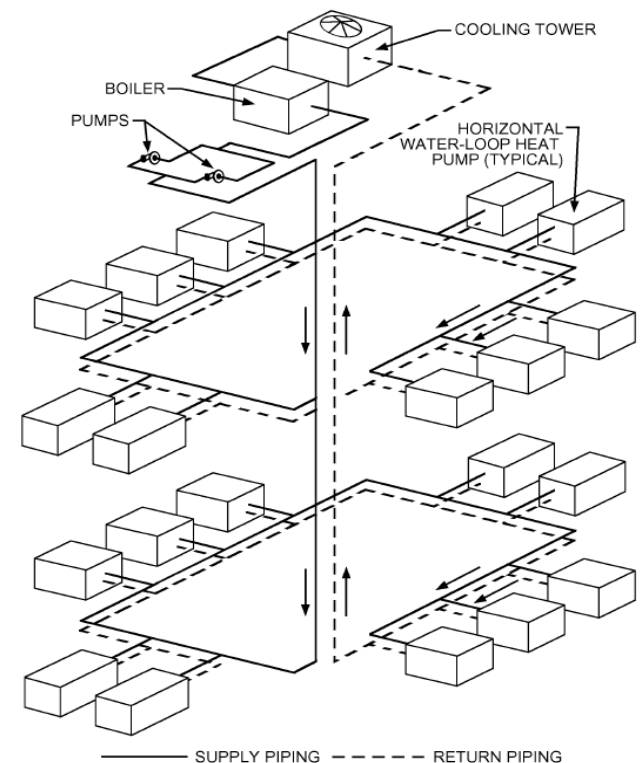
- Water-Loop Heat Pump (WLHP)
- Radiant In-Floor Heating
- Domestic Hot Water Preheat
- Winter Ventilation OA Preheat, Summer Reheat for Dehumidification
- Snow Melt (in Heating Mode or during Cooling + Desuperheater)

### MEDIUM TEMPERATURE HEATING APPLICATIONS:

- Terminal Units (Fan Coils, Cabinet Heaters, etc.)
- Central or Zoned AHU Hydronic Heating Coils
- Domestic Hot Water/Preheat



## WATER LOOP HEAT PUMP SYSTEM



**Image Source:** ASHRAE HANDBOOK: 2020 HVAC SYSTEMS AND EQUIPMENT  
Ch. 9 Fig. 30

# WHY AIR-TO-WATER HEAT PUMPS FOR HYDRONIC SYSTEMS?

## EMISSIONS COMPARISON

### MANITOBA ELECTRICITY GENERATION:

0.0011 kg CO<sub>2</sub>e /kWh

SOURCE: PROVINCIAL & TERRITOPRIAL ENERGY PROFILES – MANITOBA.

[HTTPS://WWW.CER-REC.GC.CA/EN/DATA-ANALYSIS/ENERGY-MARKETS/PROVINCIAL-TERRITORIAL-ENERGY-PROFILES/PROVINCIAL-TERRITORIAL-ENERGY-PROFILES-MANITOBA.HTML#:~:TEXT=NATIONAL%20INVENTORY%20REPORT-DESCRIPTION%3A,CO2E%20PER%20KWH.](https://www.cer-rec.gc.ca/en/data-analysis/energy-markets/provincial-territorial-energy-profiles/provincial-territorial-energy-profiles-manitoba.html#:~:text=NATIONAL%20INVENTORY%20REPORT-DESCRIPTION%3A,CO2E%20PER%20KWH.)

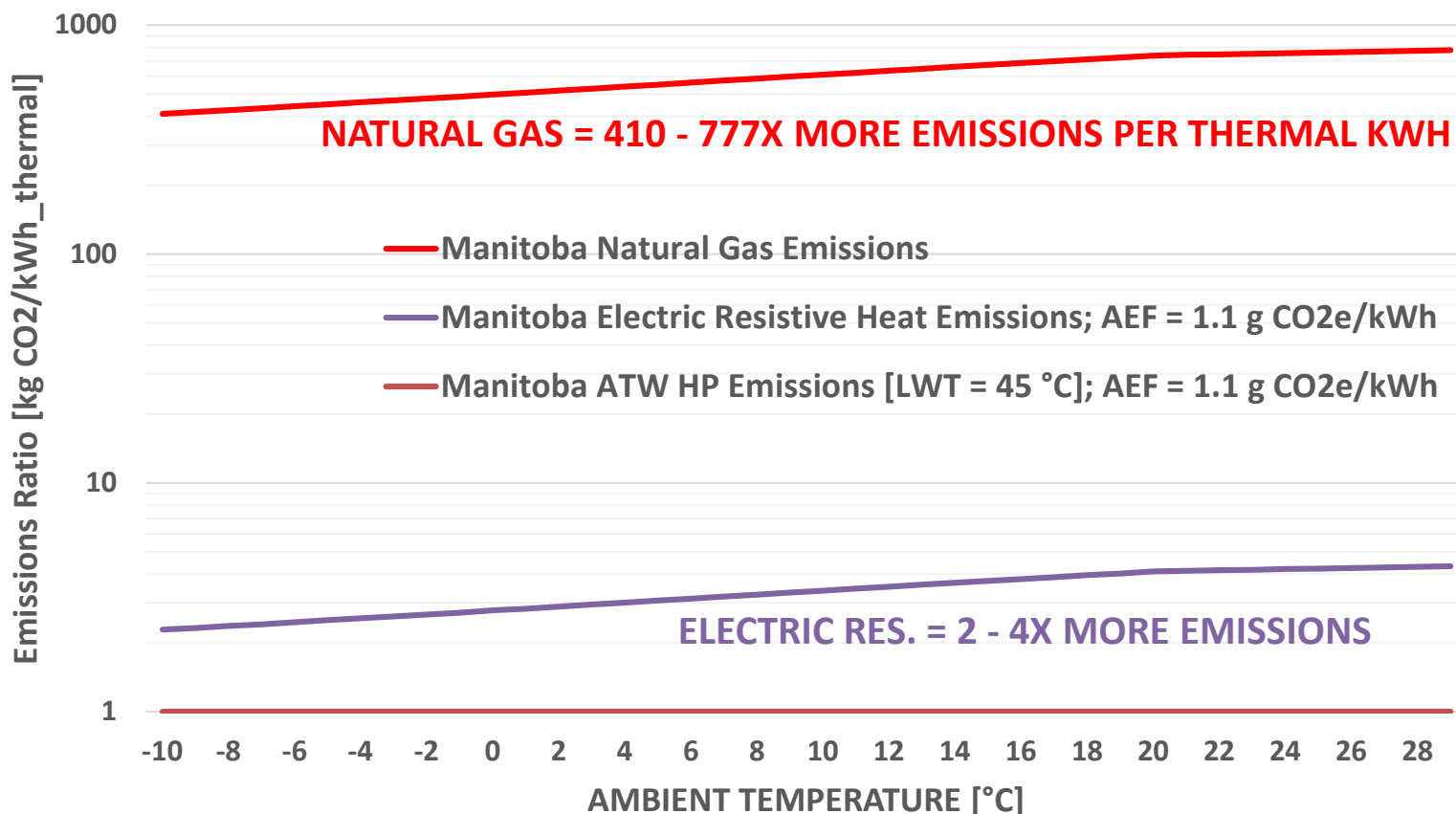
### ONTARIO NATURAL GAS EMISSION INTENSITY:

1.888 kg CO<sub>2</sub>e/m<sup>3</sup>  
= 0.18693 kg CO<sub>2</sub>e/kWh

[1 m<sup>3</sup> Natural Gas = 10.5 kWh]

SOURCE: ONTARIO MINISTRY OF ENVIRONMENT AND CLIMATE CHANGE'S "GUIDELINE FOR QUANTIFICATION, REPORTING AND VERIFICATION FOR GHG EMISSIONS - JULY 2017", TABLE 400-2

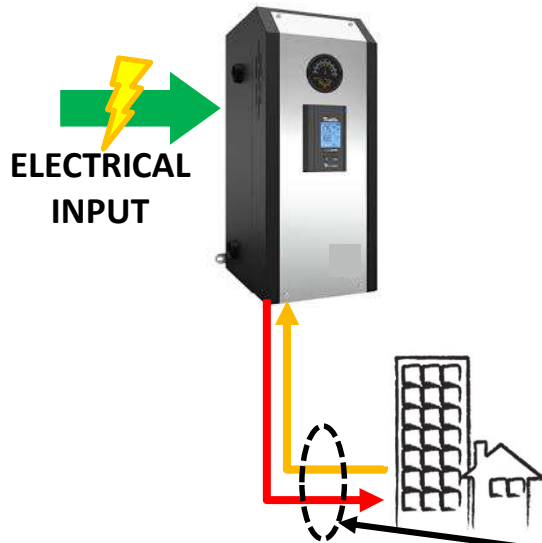
Emissions Ratio for Electric Resistive Heat, Electric Heat Pump & Natural Gas  
Manitoba: 1.1 g CO<sub>2</sub>e/kWh Annual Emission Factor (AEF)



# COP OF VARIOUS HEATING TECHNOLOGIES

## ELECTRIC BOILER

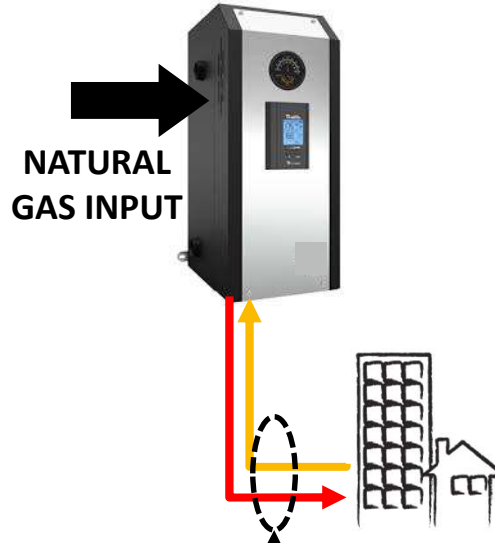
COP = 1



## CONVENTIONAL NATURAL GAS BOILER

COP < 1

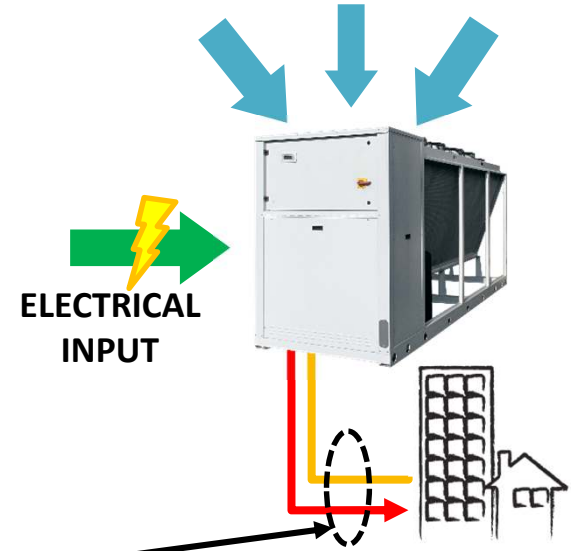
VARIES ACCORDING BOILER EFFICIENCY & SYSTEM RETURN TEMP (FOR CONDENSING GAS BOILERS)



## AIR-TO-WATER HEAT PUMP

COP = 2-4+

VARIES ACCORDING TO OUTSIDE AIR TEMP.



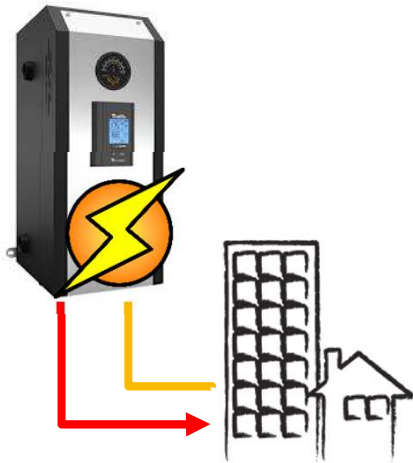
1 THERMAL kWh HEATING OUTPUT  
Hot Water For Space Heating & DHW



# CENTRAL PLANT COMPARISON FOR BACK-UP FUEL TYPES

## WHAT DOES YOUR LOW-CARBON ELECTRIFIED SOLUTION LOOK LIKE FOR HYDRONIC SYSTEMS?

### E-BOILER PRIMARY HEAT SOURCE



### 100% ELECTRIC SOLUTION:

- Requires 100% Electric Boiler @ Design Conditions
- Only COP = 1
- Higher Peak Electrical kW (Peak Capacity)
- Backup Generator Sized at Full Electric Boiler kW Load
- Excessive Demand Charges
- Significant Electrical Upgrades for Retrofits
  - Electrical Grids Cannot Support at Scale

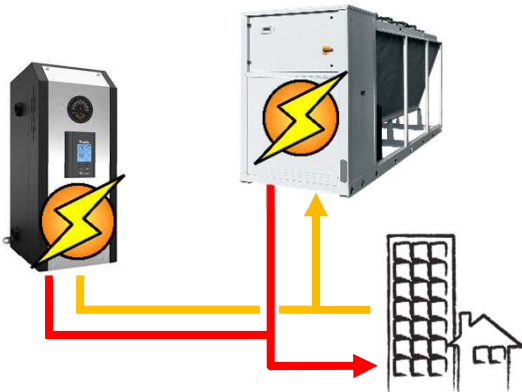
# CENTRAL PLANT COMPARISON FOR BACK-UP FUEL TYPES

## WHAT DOES YOUR LOW-CARBON ELECTRIFIED SOLUTION LOOK LIKE FOR HYDRONIC SYSTEMS?

### ATWHP + E-BOILER BACKUP

ELECTRIC  
BACKUP HEAT  
SOURCE

ATW HP  
PRIMARY  
HEAT SOURCE



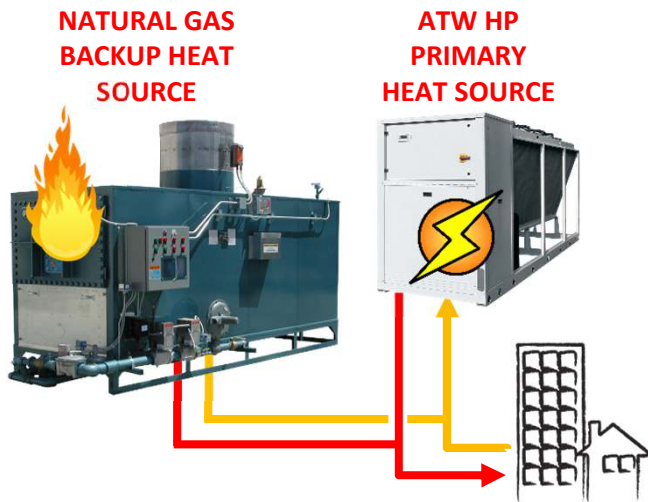
### AIR-TO-WATER HEAT PUMP + 100% ELECTRIC SOLUTION:

- Cut-out Temperature of ATW Heat Pump Requires **100% Electric Boiler BACKUP** @ Design Conditions (i.e. -30 °C)
- Use Heat Pump For Fuel Switching as Much as Possible to offset
  - Leverage fewer Hours E-Boiler will run (BIN WEATHER)
- Lower kW Input of ATW vs. E-Boiler
  - Backup Capacity still at Peak e-Boiler Peak kW @ COP of 1
- Building Energy Source Fixed to Electric (No Operating Cost Resiliency)

# CENTRAL PLANT COMPARISON FOR BACK-UP FUEL TYPES

## WHAT DOES YOUR LOW-CARBON ELECTRIFIED SOLUTION LOOK LIKE FOR HYDRONIC SYSTEMS?

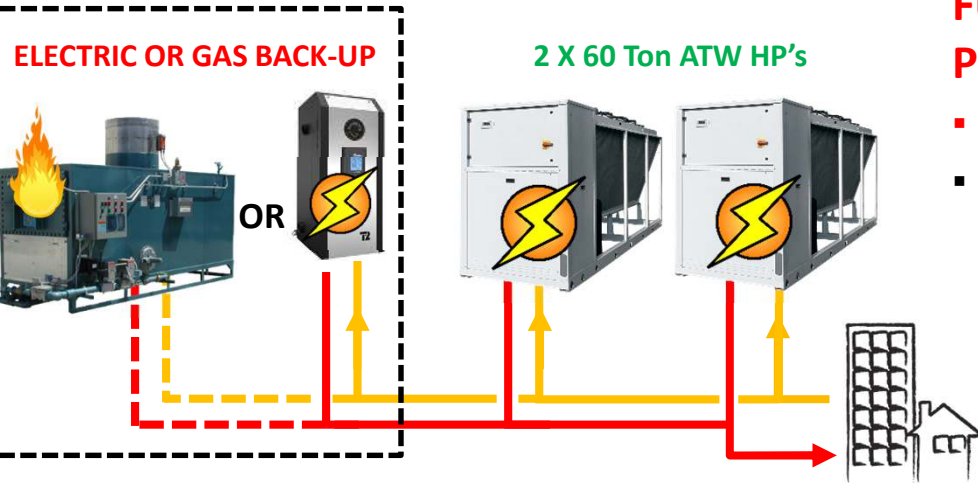
### ATWHP + NG BOILER BACKUP



### AIR-TO-WATER HEAT PUMP + BACKUP NATURAL GAS

- Cut-out Temperature of ATW Heat Pump Requires **100% Natural Gas Boiler BACKUP** @ Design Conditions
  - **Keep Existing Infrastructure, Extend Existing Boiler Life**
- Use Heat Pump For Fuel Switching as Much as Possible
  - Leverage fewer Hours NG-Boiler will run (BIN WEATHER)
- Significantly Reduced Electric Heat Pump Electrical Power Supply
  - **(2X Less due to COP)**
- **Dual Fuel System Provides Resilience & Redundancy for Operating Costs & Carbon Footprint**
- **No Backup Generator excessive sizing for Electric Boiler @ COP = 1**

# WINNIPEG, MB CENTRAL PLANT HEATING ANALYSIS EXAMPLE: 120 TON CHILLER SYSTEM (2 X 60 TON UNITS)

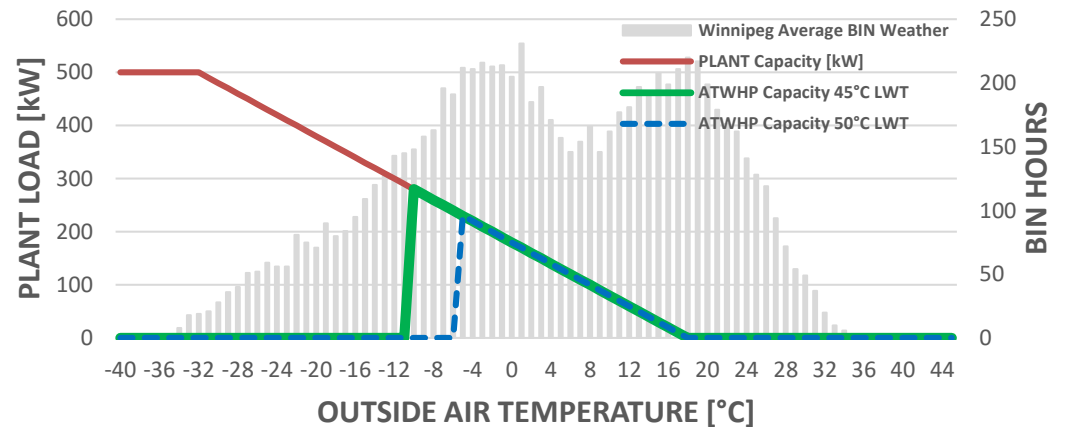


## FUEL SOURCE COMPARISON: AIR-TO-WATER HEAT PUMP + BACKUP NATURAL GAS OR ELECTRIC

- **430 kW Peak Load** Using TWO 60 Ton Air-to-Water Heat Pump Units
- Comparison for Sizing Based on -10 C and -5 C Cut-out Temperature:
  - 40% Propylene Glycol
  - 45 °C LWT / -10 °C Cut-Out →  $CAP_{RATED} = 135 \text{ kW}$ ;  $COP_{RATED} = 2.07$
  - 50 °C LWT / -5 °C Cut-out →  $CAP_{RATED} = 110 \text{ kW}$ ;  $COP_{RATED} = 2.10$

Peak Load [kW]	Ambient Temp. [°C]	Rated Capacity (Each) [kW]	Efficiency COP [W/W]
500	-38	<b>GAS OR ELECTRIC AUX.</b>	
280	-10	140	2.07
230	-5	115	2.10

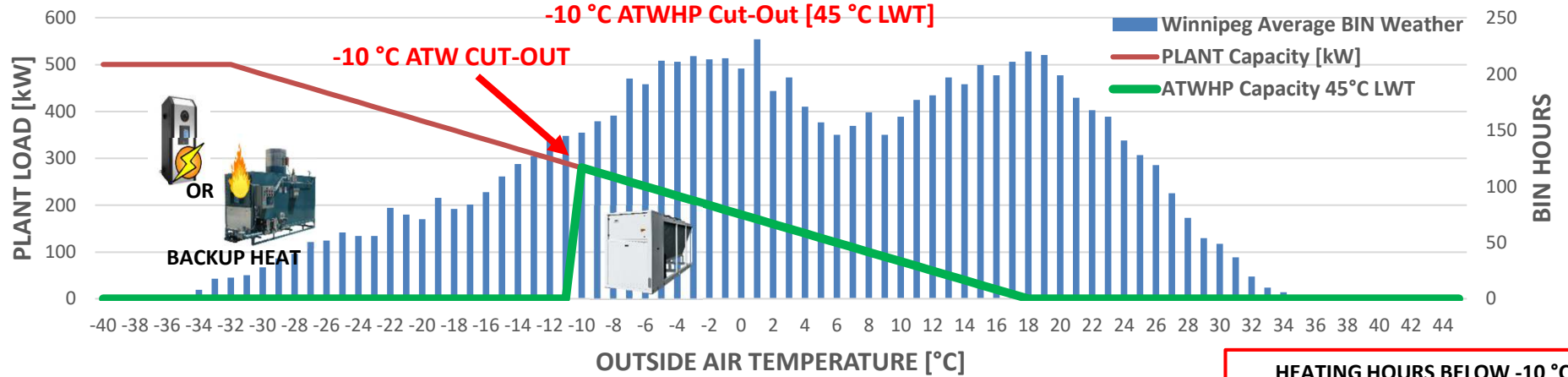
CENTRAL PLANT FUEL SOURCE & BIN HOURS



# CENTRAL PLANT COMPARISON FOR BACK-UP FUEL TYPES

## FUEL SOURCE COMPARISON CONSIDERING AIR-TO-WATER HEAT PUMP EFFICIENCIES & BACKUP FUEL USES

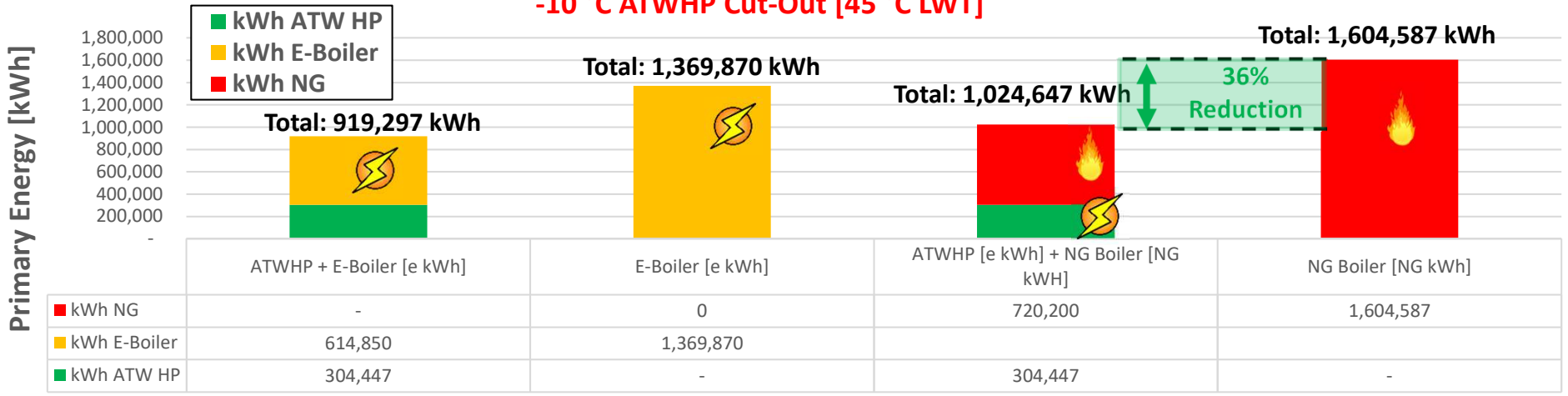
CENTRAL PLANT FUEL SOURCE & BIN HOURS



HEATING HOURS BELOW -10 °C = 1,673  
HOURS BETWEEN -10 °C to +10 °C = 3,842

## Central Plant Fuel Source Comparison: 2x 60-Ton ATW HP Units

-10 °C ATWHP Cut-Out [45 °C LWT]

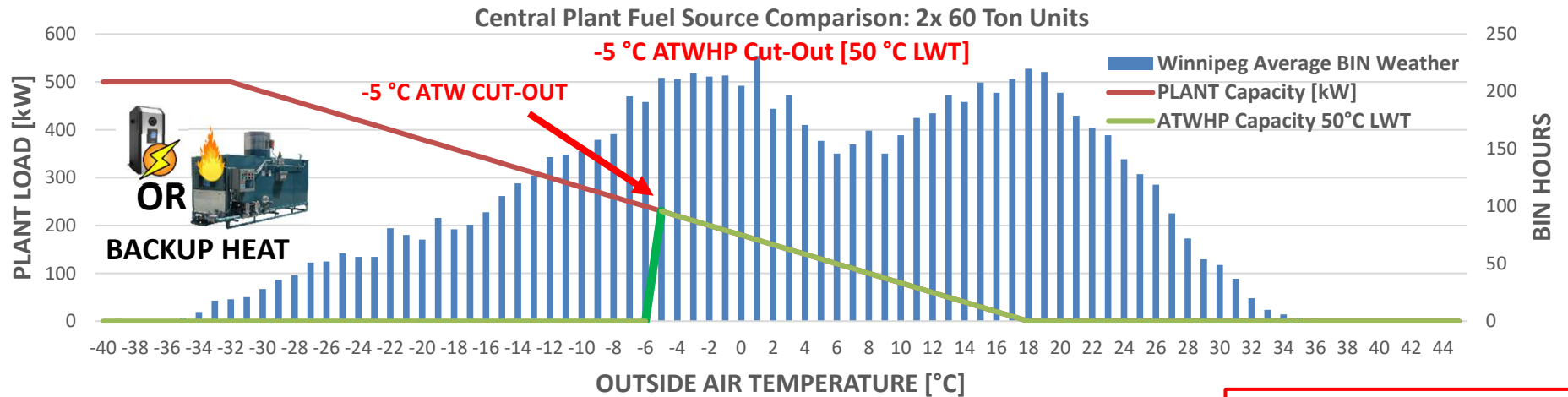


	ATWHP + E-Boiler [e kWh]	E-Boiler [e kWh]	ATWHP [e kWh] + NG Boiler [NG kWh]	NG Boiler [NG kWh]
kWh NG	-	0	720,200	1,604,587
kWh E-Boiler	614,850	1,369,870	-	-
kWh ATW HP	304,447	-	304,447	-

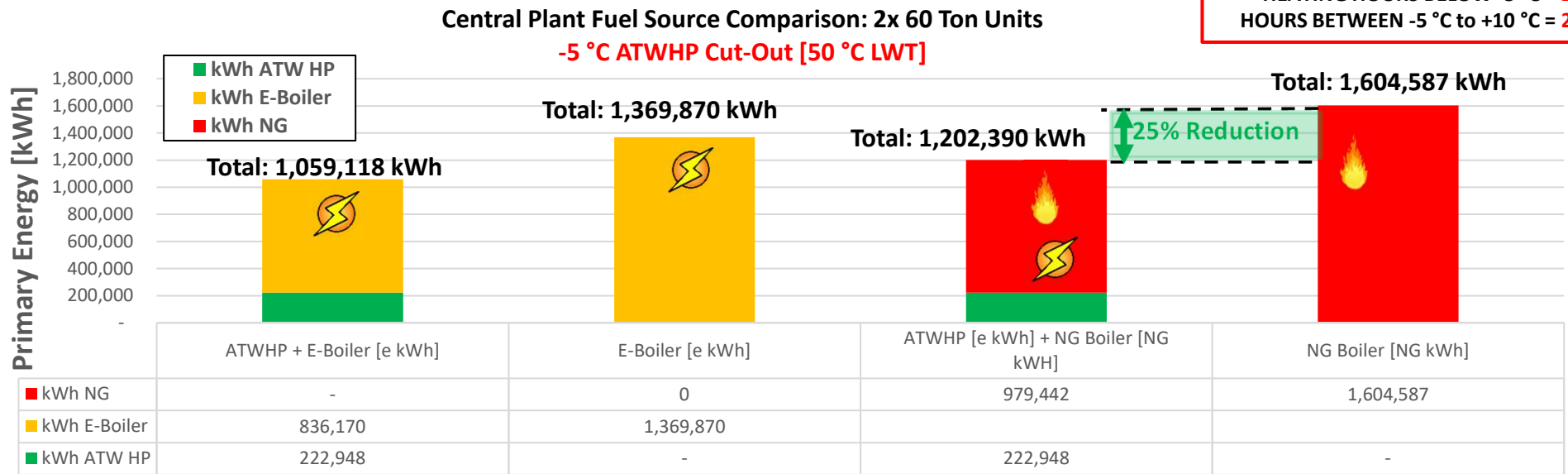
Central Plant Back-Up Type

# CENTRAL PLANT COMPARISON FOR BACK-UP FUEL TYPES

## FUEL SOURCE COMPARISON CONSIDERING AIR-TO-WATER HEAT PUMP EFFICIENCIES & BACKUP FUEL USES



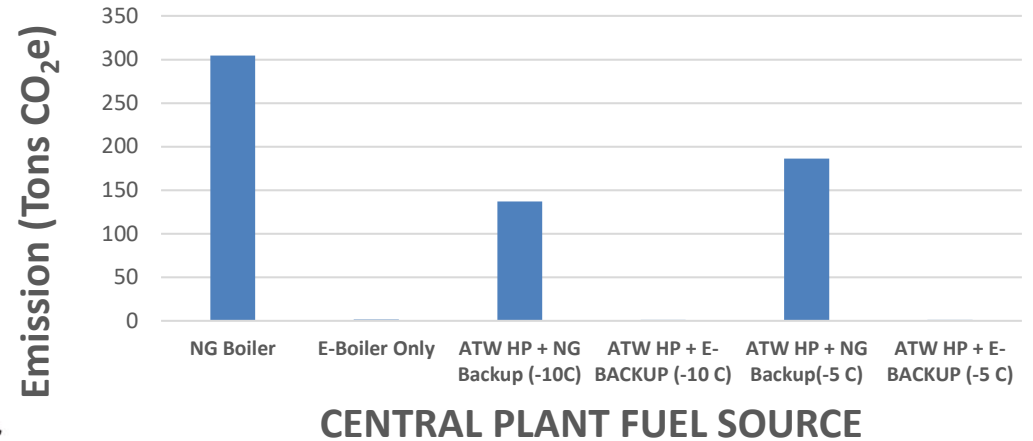
HEATING HOURS BELOW -5 °C = 2,529  
HOURS BETWEEN -5 °C to +10 °C = 2,986



Central Plant Back-Up Type

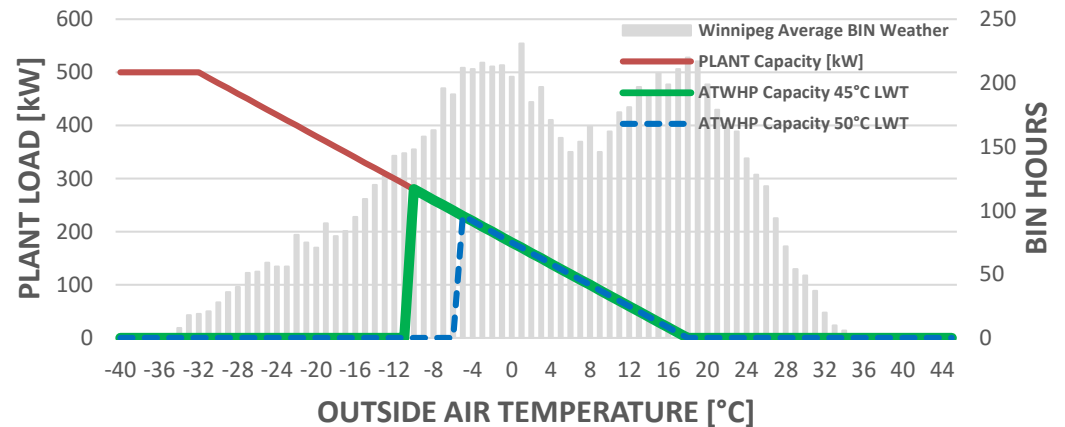
# WINNIPEG, MB CENTRAL PLANT HEATING ANALYSIS EXAMPLE: 120 TON CHILLER SYSTEM (2 X 60 TON UNITS)

Annual Emissions Fuel Source Comparison



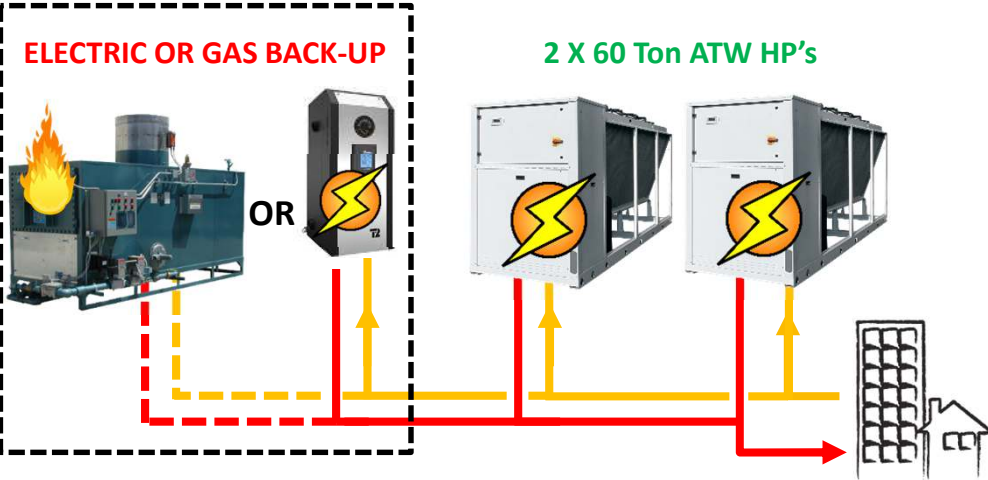
CENTRAL PLANT FUEL SOURCE

CENTRAL PLANT FUEL SOURCE & BIN HOURS



ELECTRIC OR GAS BACK-UP

2 X 60 Ton ATW HP's



Peak Load [kW]	Ambient Temp. [°C]	Rated Capacity (Each) [kW]	Efficiency COP [W/W]	Annual Tonnes CO <sub>2</sub> e Offset (Gas Backup)
500	-38	<b>GAS OR ELECTRIC AUX.</b>		-
280	-10	140	2.07	167.7
230	-5	115	2.10	118.5

# REDUCING BUILDING GHG EMISSIONS WITH AIR-TO-WATER HEAT PUMPS

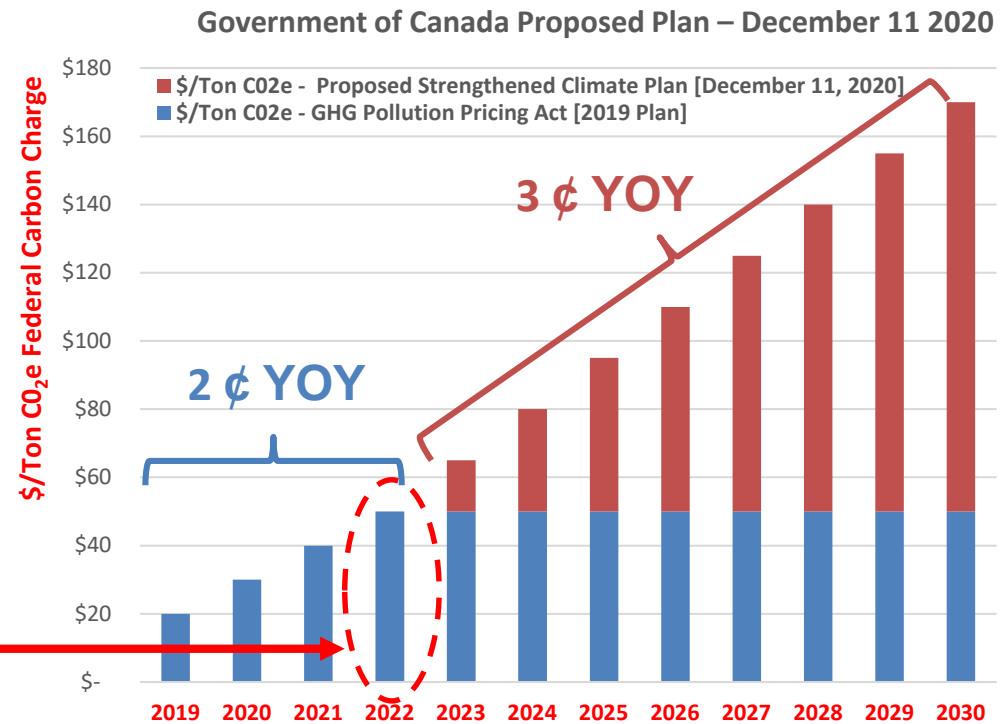
## HOW WILL FOSSIL FUEL PRICES BE AFFECTED IN A LOW-CARBON FUTURE?

### FEDERAL CARBON CHARGE: ONTARIO (ENBRIDGE)

<https://www.enbridgegas.com/Natural-Gas-and-the-Environment/Enbridge-A-Green-Future/Federal-Carbon-Pricing-Program>

2019 – 2022 Federal Carbon Charge Rates for Marketable Natural Gas

Year	\$/ tCO <sub>2</sub> e	cents/m <sup>3</sup>
2019	\$20	3.91
2020	\$30	5.87
2021	\$40	7.83
2022	\$50	9.79



**2023-2030 Will see a rise in Carbon Tax by \$15/Ton CO<sub>2</sub>e, which Translates to ~ 3 ¢ YOY**

\*\*According to the Plan, if implemented, the Carbon tax will increase by \$15/year until it reaches \$170/ton by 2030

1. Source: Ontario Ministry of Environment and Climate Change's "Guideline for Quantification, Reporting and Verification for GHG Emissions - July 2017", Table 400-2
2. Source: National Inventory Report (NRI) 1990-2014: Greenhouse Gas Sources and Sinks in Canada, Part 3

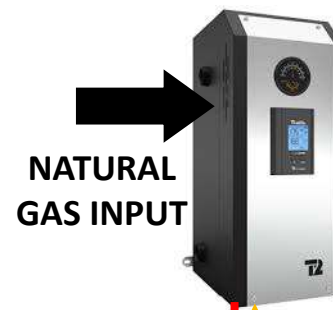


# REDUCING GHG EMISSIONS & OPERATING COSTS WITH AIR-TO-WATER HEAT PUMPS

HOW TO COMPARE 1 kWh<sub>THERMAL</sub> NATURAL GAS TO ELECTRIC HEAT PUMP?

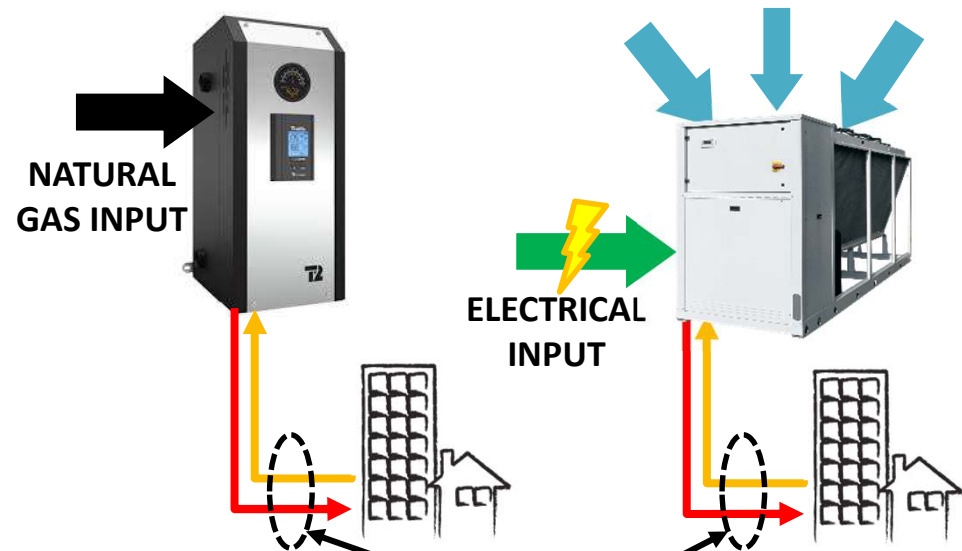
## CONVENTIONAL BOILER

Boilers Burn Fossil-Fuels to Heat Water (**NON-Renewable**)



## AIR-TO-WATER HEAT PUMP

Air-Source Heat Pumps Extract Heat from Environment (**Renewable**)



1 THERMAL kWh HEATING OUTPUT  
Hot Water For Space Heating & DHW

$$1 \text{ kWh}_{THERMAL,BOILER} = 1 \text{ kWh}_{THERMAL,HEAT PUMP}$$

$$\frac{\$/\text{kWh}_{Natural Gas}}{\text{Boiler Efficiency} [\%]} = \frac{\$/\text{kWh}_{Electrical}}{COP}$$

$$\text{Breakeven } COP_{HEAT PUMP} = \frac{\$/\text{kWh}_{Electrical}}{\$/\text{kWh}_{Natural Gas}} \times \text{Boiler Efficiency}$$

\*\*Above Arithmetic does not account for Electricity Demand Charges

# REDUCING GHG EMISSIONS & OPERATING COSTS WITH AIR-TO-WATER HEAT PUMPS

## HOW TO COMPARE 1 kWh<sub>THERMAL</sub> PROVIDED BY NATURAL GAS OR HEAT PUMP?

$$COP_{HEAT\ PUMP, Breakeven} = \frac{\$/kWh_{Electrical}}{\$/kWh_{Natural\ Gas}} \times \eta_{Boiler}$$

### MANITOBA HYDRO RATES:

1 m<sup>3</sup>NG = 10.5 kWh<sub>Natural Gas</sub>

### Average Natural Gas Price

= \$0.45/m<sup>3</sup> Approx. Total Effective Price from TOTAL of NG Bill (Based on 2022 Carbon Pricing @ \$50/Ton CO<sub>2</sub>e)

### Average Electricity Price

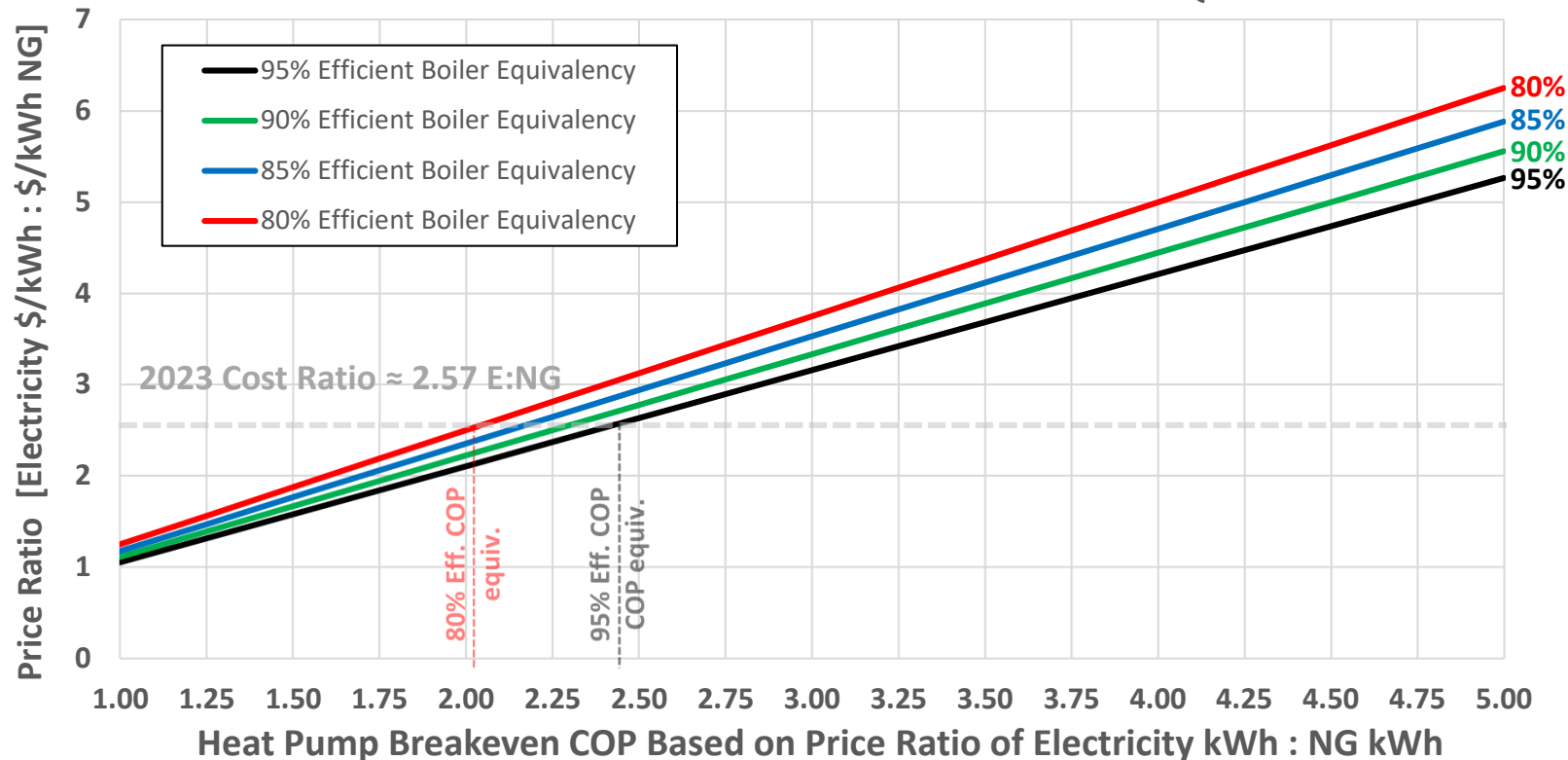
= \$0.11/kWh

2023 Cost Ratio ≈ 2.57 E:NG

Breakeven COP<sub>95%</sub> = 2.44

Breakeven COP<sub>80%</sub> = 2.05

### NATURAL GAS BOILER EFFICIENCY & HEAT PUMP EQUIVALENCY

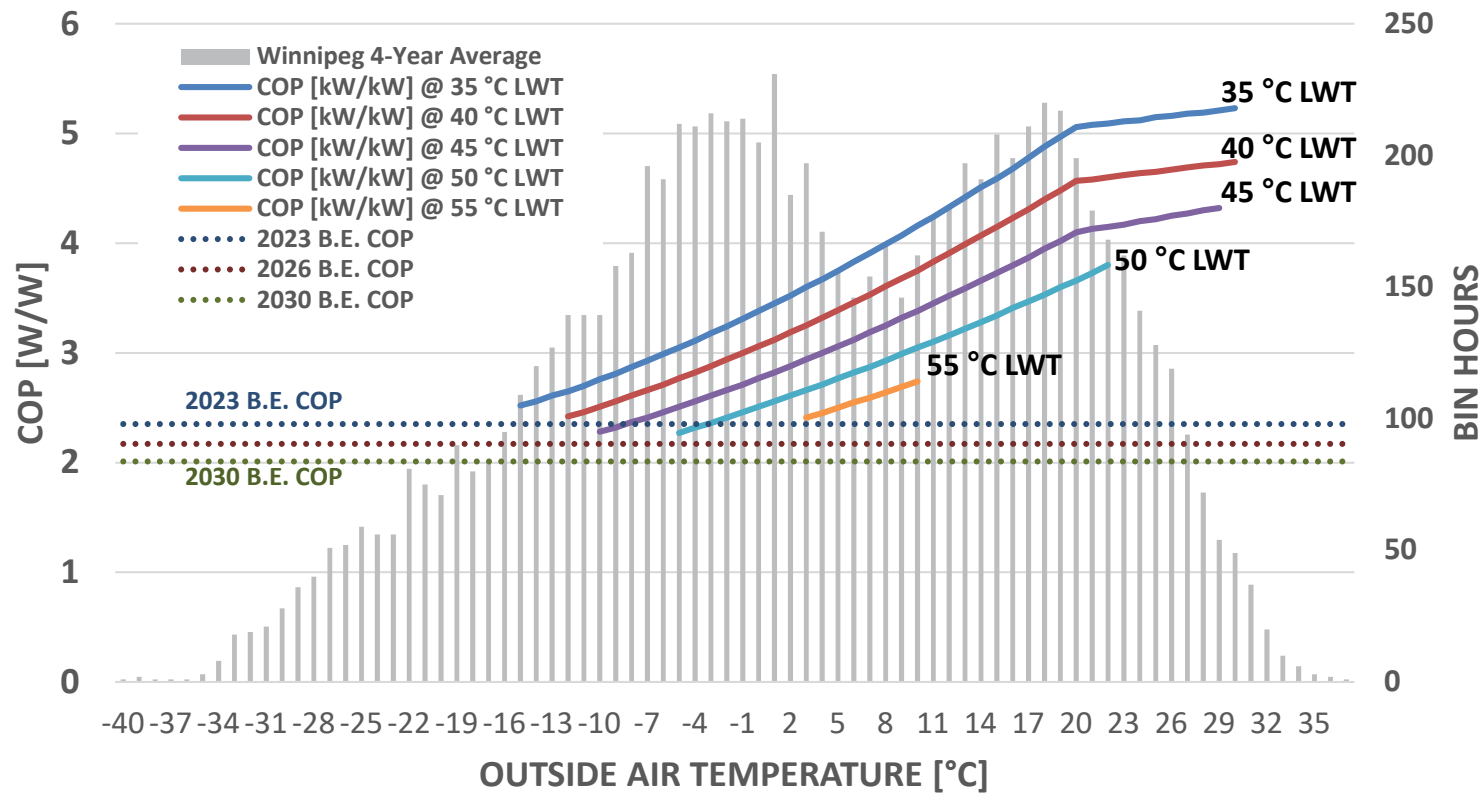


\*\*Above Arithmetic does not account for Electricity Demand Charges

# REDUCING BUILDING GHG EMISSIONS WITH AIR-TO-WATER HEAT PUMPS

## CARBON TAX IMPROVES HEAT PUMP OPERATIONAL COSTS 2022-2030

65-Ton ATW HP COP vs. OAT: WINNIPEG, MB BIN WEATHER DATA  
4-YEAR AVERAGE APRIL 2018-MARCH 2022



### Annual Average Energy Source Comparison - Manitoba

Year	Electricity Rate [\$/kWh]	Natural Gas Rate [\$/m <sup>3</sup> ]	Breakeven COP (95% Eff. Boiler)
2022	\$0.110	\$0.45	2.44
2023	\$0.113	\$0.48	2.35
2024	\$0.117	\$0.51	2.28
2025	\$0.120	\$0.54	2.22
2026	\$0.124	\$0.57	2.17
2027	\$0.128	\$0.60	2.12
2028	\$0.131	\$0.63	2.08
2029	\$0.135	\$0.66	2.04
2030	\$0.139	\$0.69	2.01

1 m<sup>3</sup> = 10.5 kWh<sub>NATURAL GAS</sub>  
Boiler Efficiency = 95%  
\$0.45/m<sup>3</sup> Natural Gas (2022)  
+ \$0.03 YOY (Carbon Tax Increase)

Avg. Electricity \$0.11/kWh (+3% YOY)

**\*\*Above Arithmetic does not account for Electricity Demand Charges**

# REDUCING BUILDING GHG EMISSIONS WITH AIR-TO-WATER HEAT PUMPS

## MANITOBA HYDRO EXAMPLE – GENERAL SERVICE (SMALL 3-PHASE) AND SMALL COMMERCIAL NATURAL GAS RATE GLASS

### NATURAL GAS:

~ \$0.1878/m<sup>3</sup> (or more) Commodity

~ \$0.1213/m<sup>3</sup> (or less) Delivery

\$0.0979 /m<sup>3</sup> (2022 Tax)

Natural Gas Bill	Amount
Total m <sup>3</sup> Usage - NG	727.54
Basic Charge	\$ 14.00
Total Commodity + Delivery of NG	\$ 240.85
Fed Carbon Charge	\$ 71.23
<b>Subtotal (incl. Fed. Carbon Charge)</b>	<b>\$ 326.08</b>
Taxes	\$ 34.15
<b>Total Bill (Incl Taxes)</b>	<b>\$ 360.23</b>
<b>Total \$/m<sup>3</sup> NG (Pre-Tax, Incl. Fed Carbon Charge)</b>	<b>\$ 0.45</b>

Natural Gas - Small Commercial / Gaz Naturel - Commercial - petit											
Meter number / N° de compteur	Service / Pour la période From / Du	To / Au	Meter readings / Relevés du compteur			Usage / Consommation	Base pressure adj/Facteur de la pression de base	Metric conversion factor/Facteur de conversion métrique	Cubic metres (m <sup>3</sup> ) / Mètres cubes (m <sup>3</sup> )	Reading type / Type de relevé	
			Days / Jours	Previous / Précédent	Present / Nouveau						
1064050	Jan 20 JAN/23	Feb 17 FÉV/23	28	257	517	260	x 0.98780	x 2.832784	=	727.538	Estimated Estimatif
Basic Charge / Redevance de base										\$ 14.00	
Gas Commodity (Centra) / Gaz - prix du produit						318.696 m <sup>3</sup>	x \$ 0.23960			76.36	
Gas Commodity (Centra) / Gaz - prix du produit						408.842	x 0.18780			76.78	
Delivery / Livraison						318.696	x 0.11960			38.12	
Delivery / Livraison						408.842	x 0.12130			49.59	
Subtotal / Total partiel										254.85	
7.00% Prov Tax / Taxe prov.										17.84	
5.00% GST / TPS										12.75	
Federal Carbon Charge / Redevance fédérale sur le carbone - 727.538 m <sup>3</sup> x \$ 0.0979										71.23	
5.00% GST on Federal Carbon Charge / TPS sur Redevance fédérale sur le carbone										3.56	
<b>Natural gas charges / Frais de gaz naturel</b>										<b>360.23</b>	

# REDUCING BUILDING GHG EMISSIONS WITH AIR-TO-WATER HEAT PUMPS

## MANITOBA HYDRO EXAMPLE – GENERAL SERVICE (SMALL 3-PHASE)

## AND SMALL COMMERCIAL NATURAL GAS RATE GLASS

### ELECTRICITY:

NON-DEMAND RATE

LESS Than \$0.095/kWh

Use \$0.11 to be Conservative

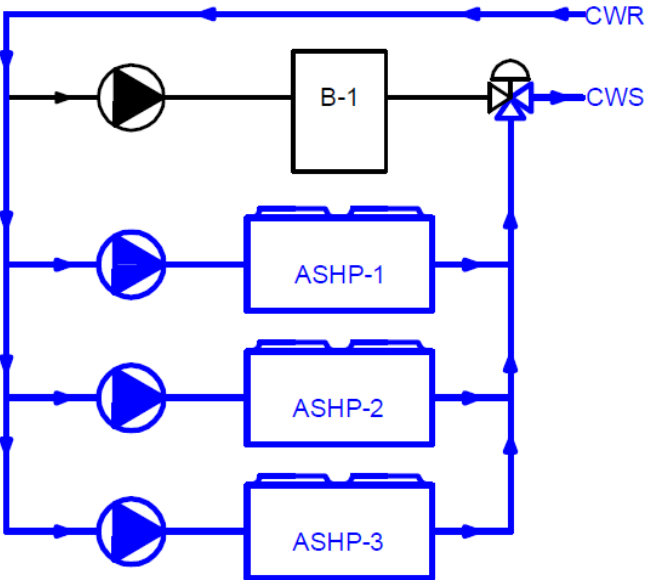
Electricity - General service small 3 phase / Électricité - Service général triphasé - petite puissance								
Meter number / N° de compteur	Service / Pour la période From / Du To / Au		Days / Jours	Meter readings / Relevés du compteur Previous / Précédent Present / Nouveau		Multiplier / Multiplicateur	kW.h / kWh	Reading type / Type de relevé
944519	Jan 20 JAN/23	Feb 17 FÉV/23	28	24397	24711	1	314	Estimated Estimatif
Basic Charge / Redevance de base							\$ 33.69	
Energy Charge / Frais d'énergie							314.000 kW.h x \$0.09485	29.78
Subtotal / Total partiel								63.47
5.00% City Tax / Taxe mun.								3.18
7.00% Prov Tax / Taxe prov.								4.44
5.00% GST / TPS								3.17
5.00% GST on City Tax / TPS sur taxe mun								0.15
<b>Electricity charges / Frais d'électricité</b>								<b>74.41</b>

# AIR-TO-WATER CENTRAL PLANT: APPLICATIONS

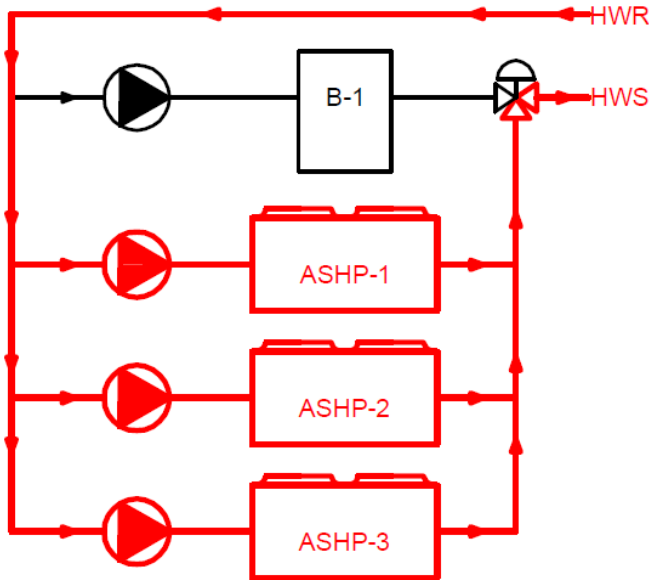
- **2-PIPE SYSTEMS:**
  - Simple 2-Pipe Change-Over System
  - Cascade Systems
- **4-PIPE HYBRID SYSTEMS** using ATW Heat Pumps
- **PARTIAL HEAT RECOVERY** in 2-Pipe & 4-Pipe Systems (Desuperheater)
- **DOMESTIC HOT WATER**

# CENTRAL HEAT PUMP PLANT: 2-PIPE CHANGEOVER COMMERCIAL SYSTEM

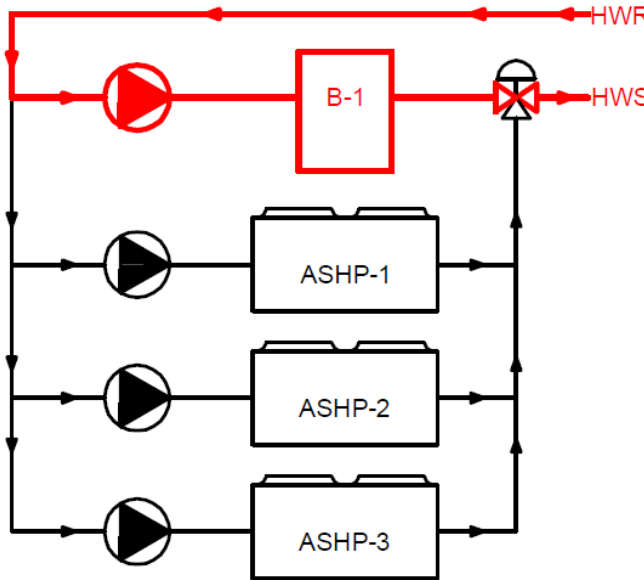
SUMMER COOLING



WINTER HEATING  
AIR-TO-WATER HEAT PUMP



WINTER HEATING  
AUXILIARY BOILER

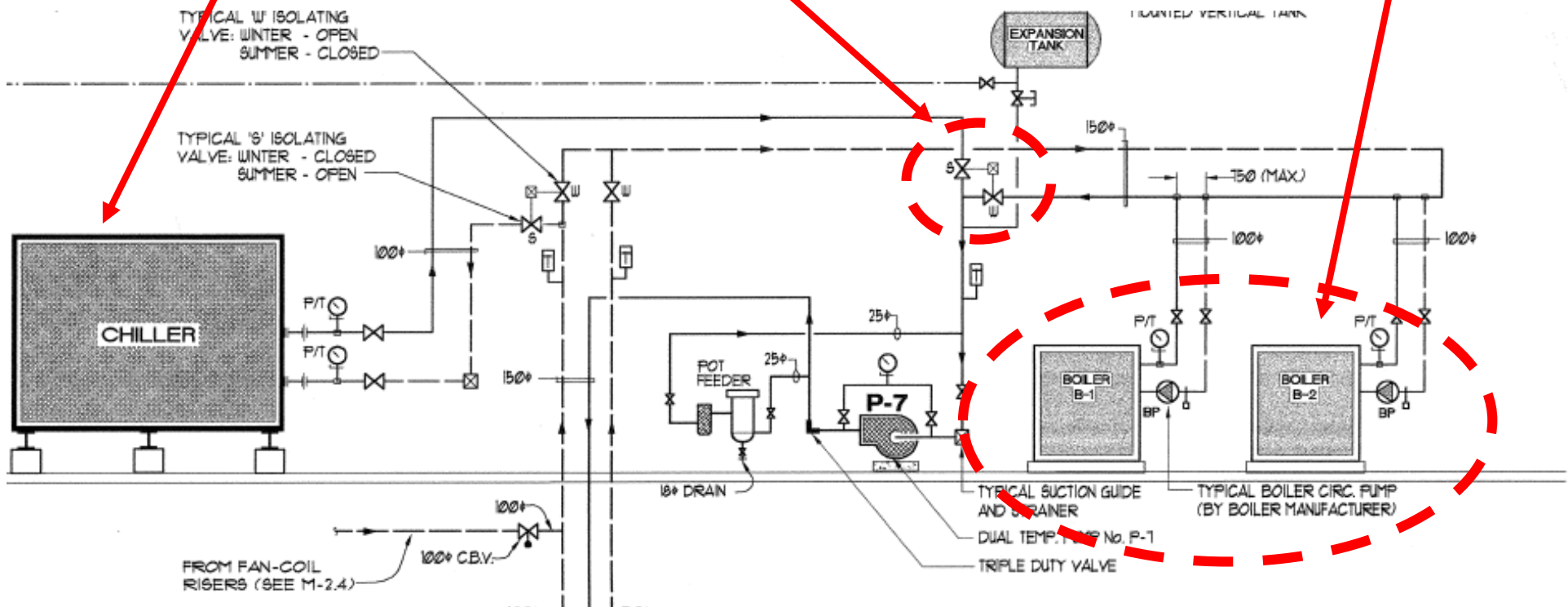


# FQSF CHILLER UPGRADE: EXISTING CHILLER SYSTEM

Chiller Drained in Winter  
(No Glycol in System)

Seasonal  
Changeover Valve

Chiller Drained in Winter  
(No Glycol in System)





# FQSF CHILLER UPGRADE: HYBRID CENTRAL HEAT PUMP PLANT

## GLYCOL SIDE

AIR-TO-WATER HEAT PUMPS  
EXTERIOR GLYCOL LOOP



HP-1: 55-Ton Nominal Cooling  
191 kW @ 8.3 °C OAT  
116 kW / 396 MBH @ -10 °C OAT  
COP = 2.03 @ -10 °C OAT



HP-2: 65-Ton Nominal Cooling  
248 kW @ 8.3 °C OAT  
155 kW / 396 MBH @ -10 °C OAT  
COP = 2.15 @ -10 °C OAT



HEAT EXCHANGERS TO DECOUPLE GLYCOL

BUFFER TANKS FOR HEAT PUMP  
COMPRESSORS



# TORONTO MURB CHILLER UPGRADE



# TORONTO MURB CHILLER UPGRADE



55-Ton ATW HP  
Same Size as  
110-Ton Std.  
Chiller

# COST BENEFIT ANALYSIS: FUEL SWITCHING RETROFIT

## PROJECT COST SUMMARY

- “Like-for-Like” Scenario based on Budgeted Reserve Fund Study of ageing chiller
- Allowance in reserve fund study for upgraded controls
- Boiler portion from reserve fund applied for retrofit as ATW Heat Pump acts as a boiler in winter.
- Reversible ATW Heat Pump project costs is actual costs at time of tender, including Engineering, Mechanical contractor, Equipment
- Incentives includes:
  - The Atmospheric Fund (TAF) Special Contribution
  - Enbridge Incentive
  - IESO Chiller Rebate (Based on NX-N exceeding IPLV requirement)
- Not captured in incentives/contributions is TRCA’s STEP Program for measurement & verification
- Anticipated more funding to be available to support similar projects based on Fuel Switching incentives and Enbridge Custom Program, Federal/Provincial Funding Programs

Like-for-Life Budget (Reserve Fund)	
Description	Amount
Air-Cooled Chiller Replacement	\$ 300,000
Heating Boilers - Secondary	\$ 80,000
Mechanical Control System	\$ 20,000
<b>Total:</b>	<b>\$ 400,000</b>

Reversible ATW Central Plant Upgrade	
Description	Amount
Reversible ATW Heat Pumps (Equipment)	\$ 220,000
Installation, Engineering Fees & Ancillary Equipment (Controls, Pumps, Heat Exchangers, Buffer Tanks)	\$ 386,200
<b>Subtotal-Fuel Switch Budget</b>	<b>\$ 606,200</b>

Project Incremental Costs - Chiller Upgrade/Fuel Switch	
<b>Incremental Cost: (Equipment+Install only)</b>	<b>\$ 206,200</b>
<b>Incentives - Actuals</b>	<b>\$ 46,500</b>
<b>Incremental Cost: (Equipment+Install only), Incl. Incentives</b>	<b>\$ 159,700</b>

# SIMPLE PAYBACK ANALYSIS: FUEL SWITCHING RETROFIT

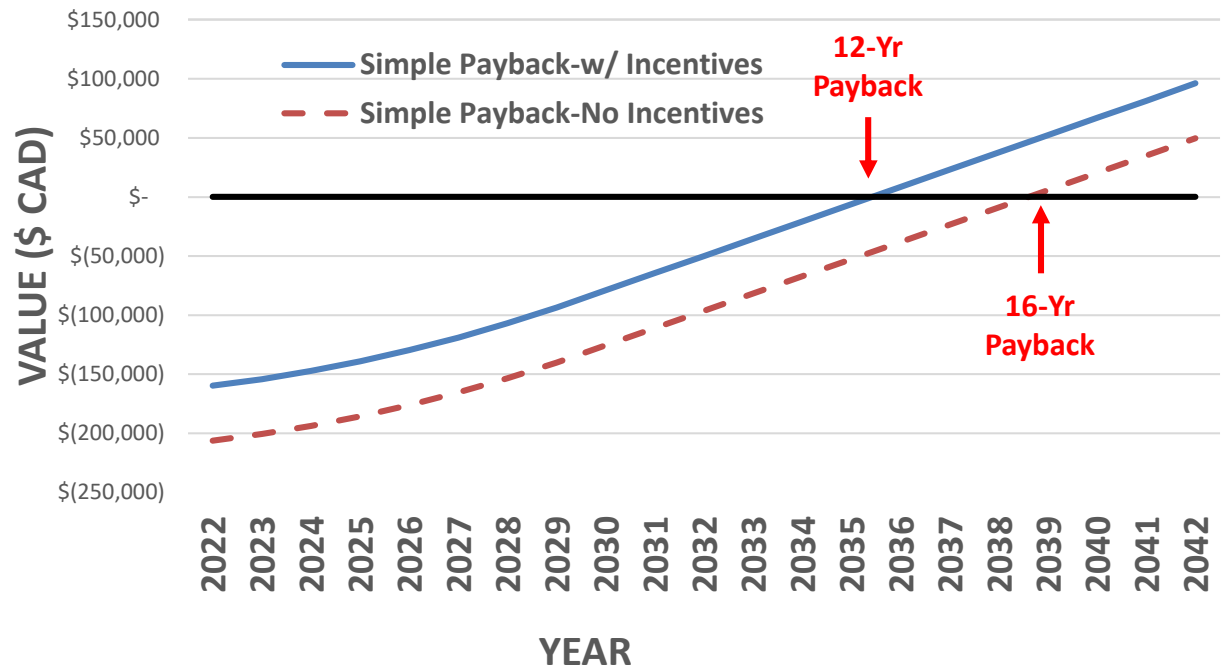
## ENERGY SAVINGS

- 45,472 m<sup>3</sup> Natural Gas Annual Savings  
Approved by Enbridge for Custom Incentive
- 85.9** Tons CO<sub>2</sub>e Emissions Offset per year  
(1.888 kg CO<sub>2</sub>e/m<sup>3</sup> Natural Gas)

Project Incremental Costs - Chiller Upgrade/Fuel Switch	
Incremental Cost: (Equipment+Install only)	\$ 206,200
Incentives - Actuals	\$ 46,500
<b>Incremental Cost: (Equipment+Install only), Incl. Incentives</b>	<b>\$ 159,700</b>

Year	\$/Ton CO <sub>2</sub> e Carbon Tax	Annau Avoided Carbon Tax	Cumulative Savings
2023	\$ 65	\$ 5,584	\$ 5,584
2024	\$ 80	\$ 6,872	\$ 12,456
2025	\$ 95	\$ 8,161	\$ 20,616
2026	\$ 110	\$ 9,449	\$ 30,065
2027	\$ 125	\$ 10,738	\$ 40,803
2028	\$ 140	\$ 12,026	\$ 52,829
2029	\$ 155	\$ 13,315	\$ 66,143
2030	\$ 170	\$ 14,603	\$ 80,746
2031	\$ 170	\$ 14,603	\$ 95,349
2032	\$ 170	\$ 14,603	\$ 109,952
2033	\$ 170	\$ 14,603	\$ 124,555
2034	\$ 170	\$ 14,603	\$ 139,158
2035	\$ 170	\$ 14,603	\$ 153,761
2036	\$ 170	\$ 14,603	\$ 168,364
2037	\$ 170	\$ 14,603	\$ 182,967
2038	\$ 170	\$ 14,603	\$ 197,570

## Chiller Upgrade to Reversible ATW Heat Pumps Simple Payback based on Carbon Tax Savings



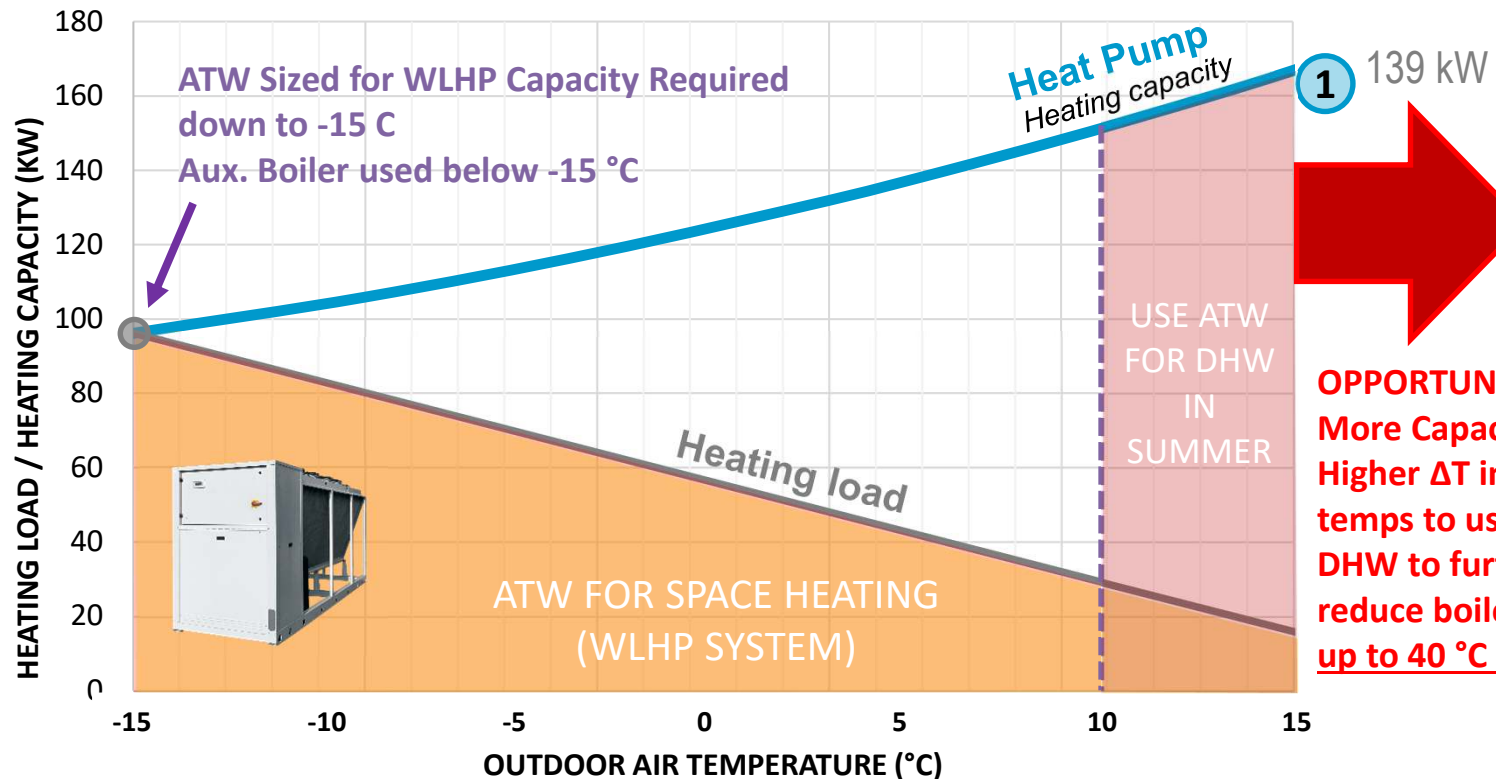
\*Savings above are estimates based on natural gas reduction. Does not account for increased efficiencies in summer due to better performance. Performance optimization may contribute to better long-term savings, TBD during M&V.

# AIR-TO-WATER HEAT PUMP: SIZING FOR HEATING

## HEATING CAPACITY VS HEATING LOAD

138 kW ATW HP (NOMINAL)

REVERSIBLE UNIT, AIR SOURCE FOR OUTDOOR INSTALLATION



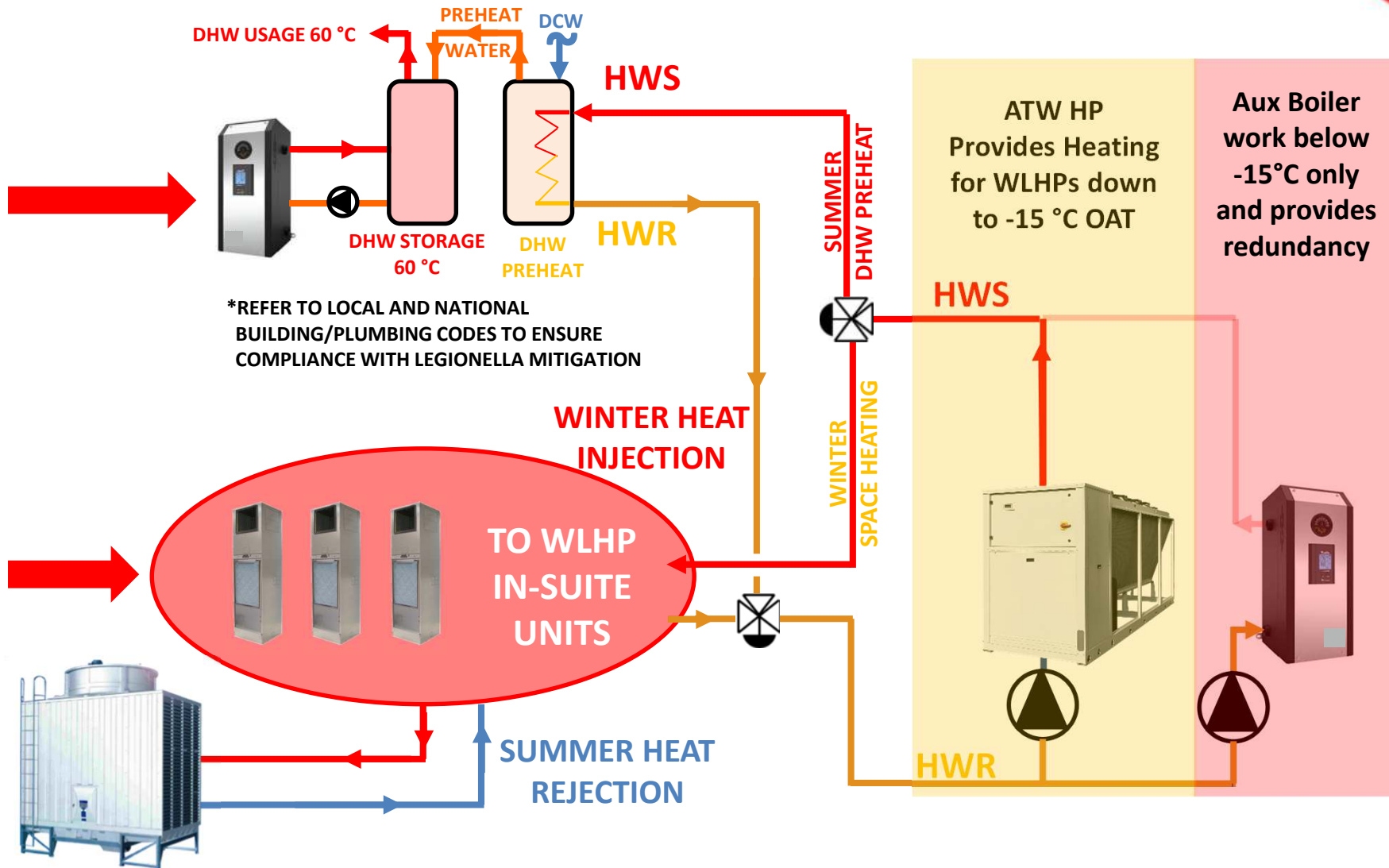
Aux. Boiler

**OPPORTUNITY:**  
More Capacity & Higher  $\Delta T$  in warmer temps to use ATW for DHW to further reduce boiler usage, up to 40 °C OAT

# MAXIMIZING ATW HP USAGE FOR DECARBONIZATION: DHW PREHEATING IN SUMMER

## SUMMER:

Since ATW HP Not Needed in Summer (Fluid Cooler), put ATW HP to work to supplement DHW Natural Gas Usage with **DHW PREHEAT**



## WINTER:

ATW HP Acts as Heat Injector in Winter to serve the WLHP System

# MAXIMIZING ATW HP USAGE FOR DECARBONIZATION: DHW PREHEATING IN SUMMER

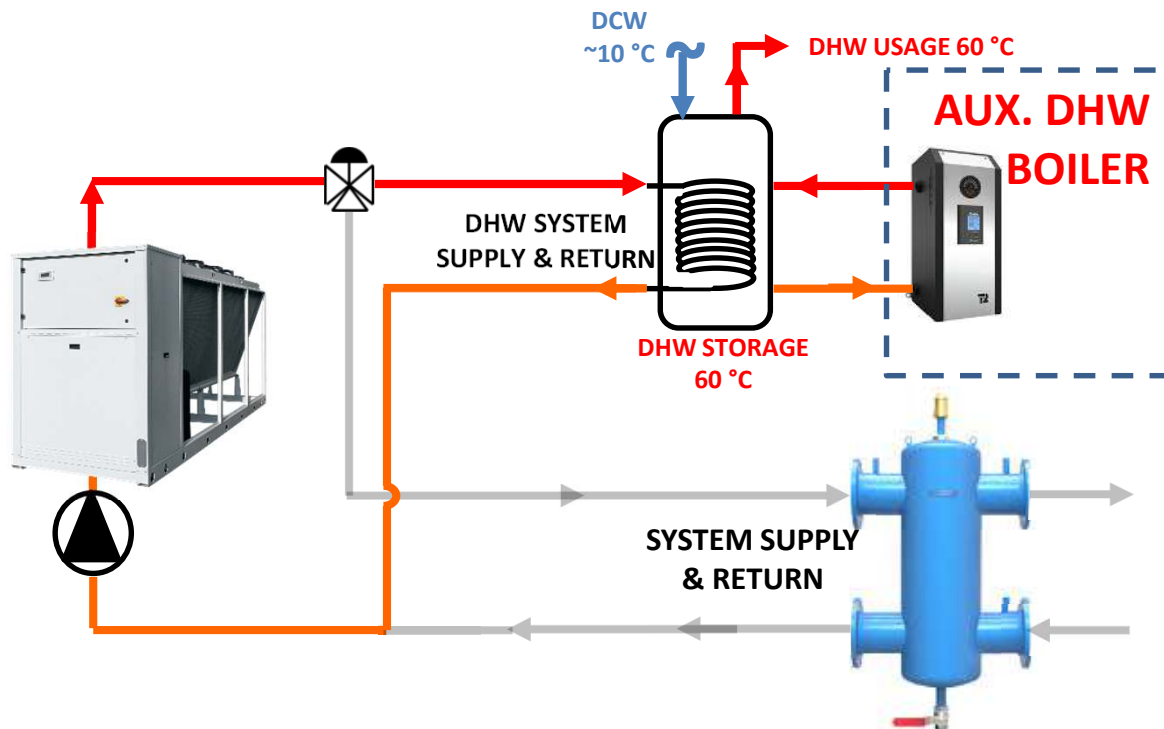
WINTER SPACE HEATING DESIGN CONDITIONS VS. SUMMER HEAT PUMP OPERATION:  
65-Ton (225 kW Cooling Cap.) Reversible Heat Pump Chiller (250 kW Heating Capacity at Std. AHRI 550 Conditions)

Design Parameter	Winter Design Conditions	Summer DHW Preheating Performance	
Fluid	40% Propylene Glycol Solution		
Flow Rate [L/s]	7.269		
Service	Space Heating	Summer DHW Preheating	
Ambient Design Temp [°C]	-15	20	30
Design Supply Water Temp [°C]	35	40	40
Temperature Difference $\Delta T$ [°C]	5	12.1	
Capacity @ 100% Load [kW]	139.5	337.6 [+242%]	
COP [W/W]	2.385	4.373 [+183%]	4.532 [+190%]



# DOMESTIC HOT WATER PRODUCTION

## DOMESTIC HOT WATER USING INDIRECT STORAGE TANK + SUPPLEMENTAL BOILER



After 50% Draw  
from DHW Tank:

$$T_{\text{TANK}} = \sim 35 \text{ }^{\circ}\text{C}$$

Can Add Heat to DHW  
with  $\sim 40 \text{ }^{\circ}\text{C}$  LWT. Can  
Use HP down to  $\sim -12 \text{ }^{\circ}\text{C}$   
OAT

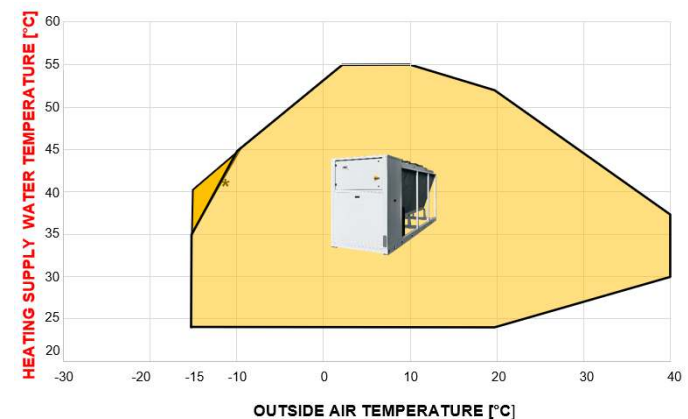
After 25% Draw  
from DHW Tank:

$$T_{\text{TANK}} = \sim 47.5 \text{ }^{\circ}\text{C}$$

Can Add Heat to DHW  
with  $\sim 52 \text{ }^{\circ}\text{C}$  LWT. Can  
Use HP down to  $\sim -3 \text{ }^{\circ}\text{C}$   
OAT only

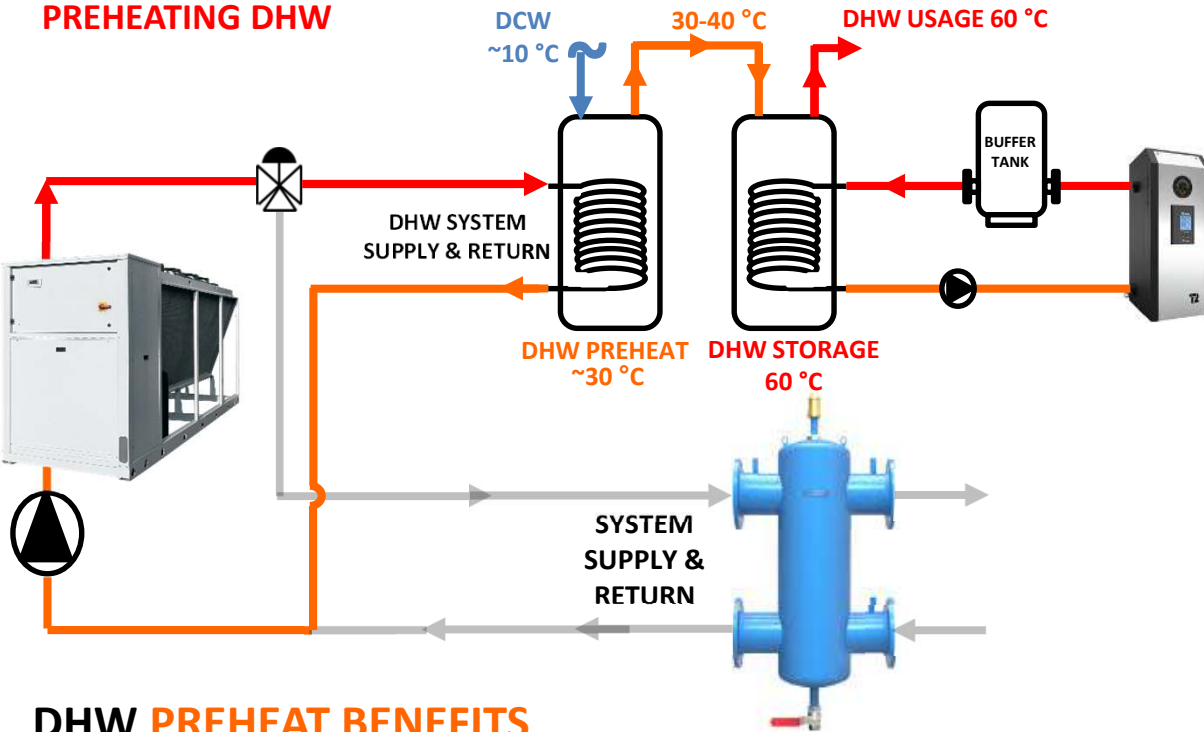
### ATW HP for DHW Application:

- Reduce Boiler work via Heat Pump
- Ability of Heat Pump to Add Heat to DHW tank is a function of DHW Tank Temp and Max LWT available from ATWHP according to OAT



# DOMESTIC HOT WATER PRODUCTION

## DOMESTIC HOT WATER USING INDIRECT STORAGE TANK FOR PREHEATING DHW



## DHW PREHEAT BENEFITS

- Reduce Boiler work via Heat Pump
- Preheat Configuration allows the heat pump to add more heat, more often to the DHW system by operating at a lower temperature. Overall offsets more GHG Emissions
- Secondary DHW Tank, boiler then does a lower temperature lift

## Looking at the PREHEAT Tank:

After 50% Draw  
from DHW  
Preheat Tank:  
 $T_{TANK} = \sim 20\text{ °C}$



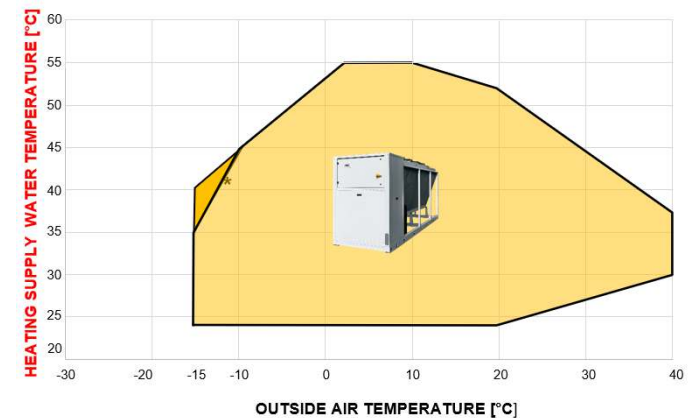
Can Add Heat to DHW  
Preheat with ~ 25 °C  
LWT. Can Use HP down  
to ~ -15 ° OAT

With pre-heated water @ 30 °C, DHW Tank does not drop below 45 °C

After 25% Draw  
from DHW Tank:  
 $T_{TANK} = \sim 24.5\text{ °C}$

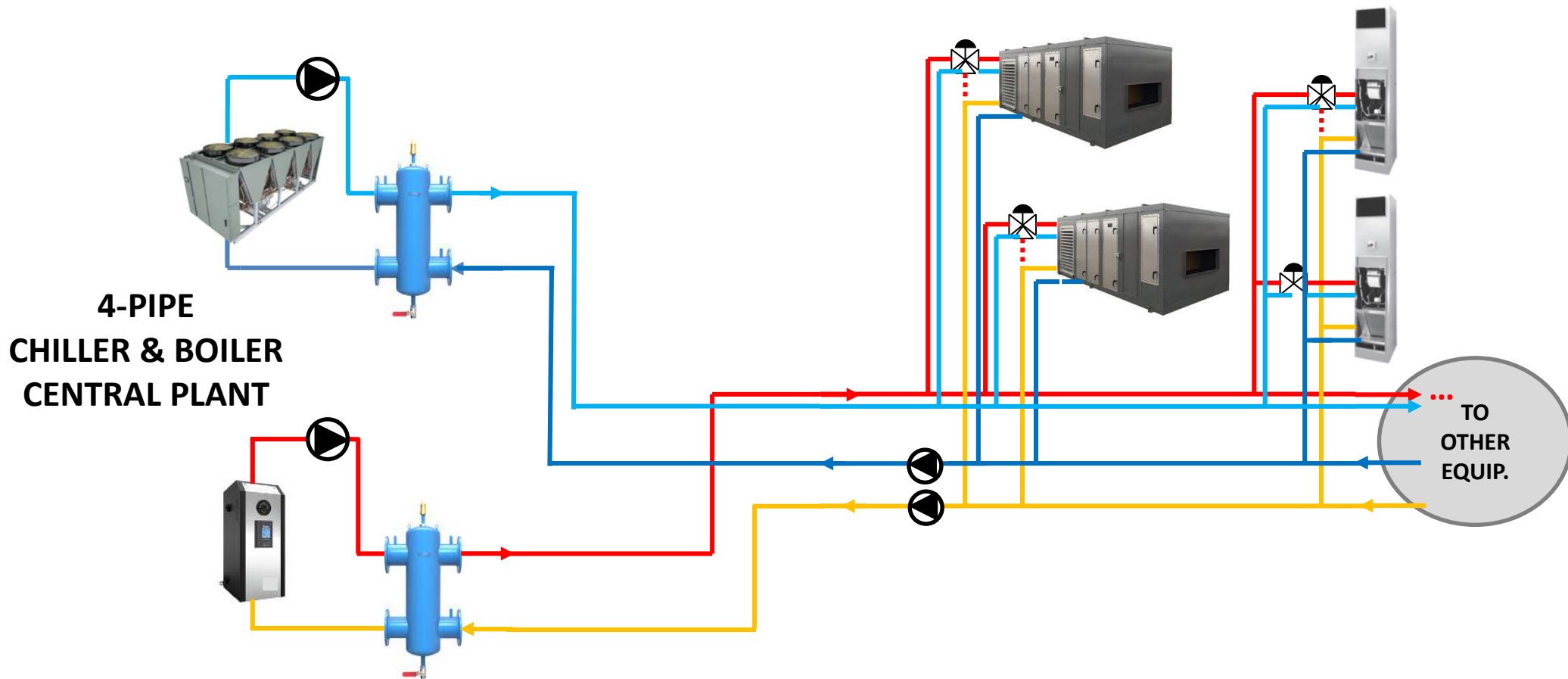


Can Add Heat to DHW  
with ~ 30 °C LWT. Can  
Use HP down to ~ -15 °C  
OAT always



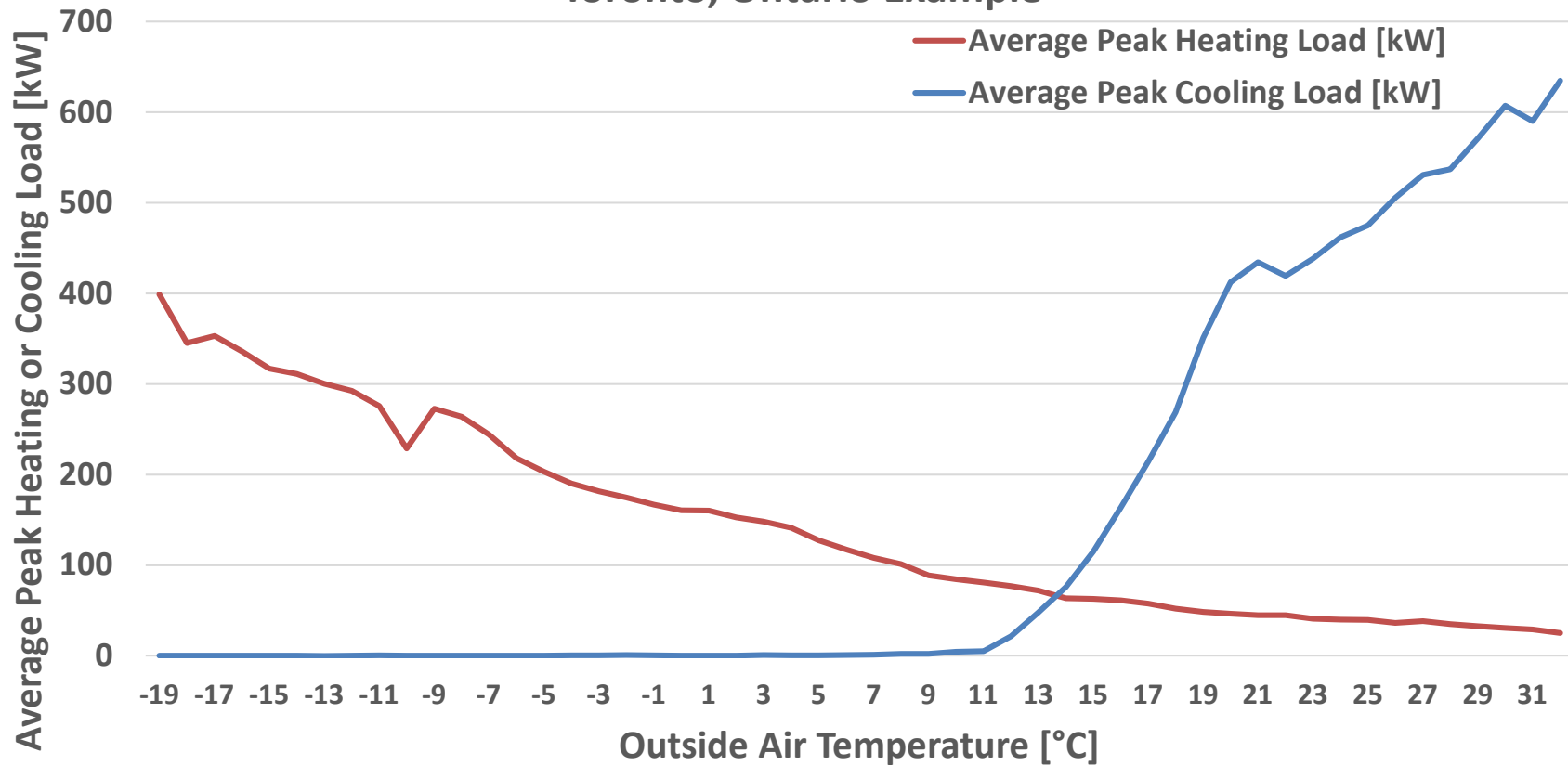
# 4-PIPE FUEL SWITCH RETROFIT

WHAT ABOUT 4-PIPE SYSTEMS?

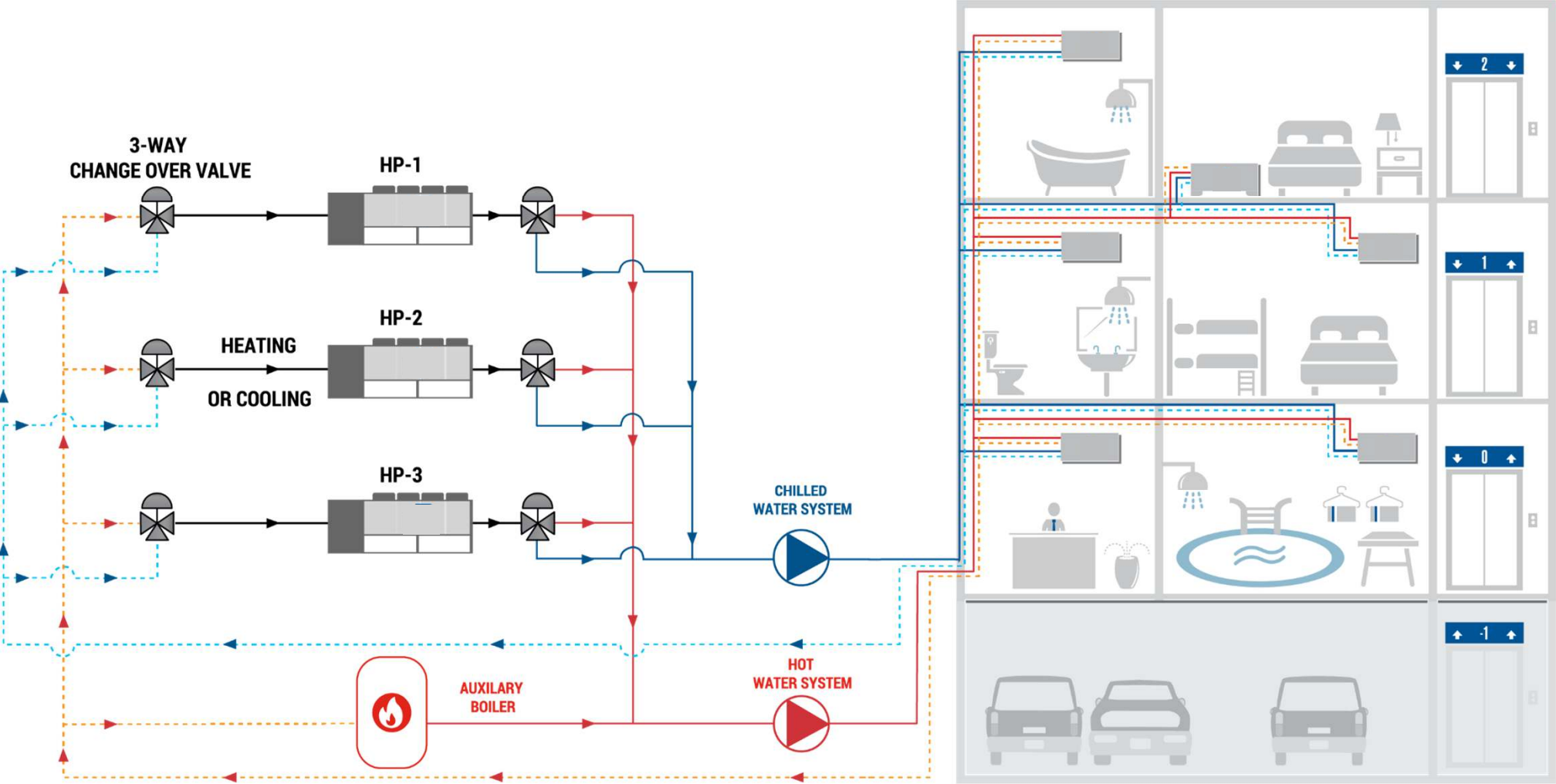


# 2-PIPE AIR-TO-WATER HEAT PUMPS IN 4-PIPE SYSTEMS

Peak Heating & Cooling Load Profiles  
Based on Average Loads at Given Outside Air Temperature  
Toronto, Ontario Example



# 4-PIPE FUEL SWITCH RETROFIT: ENERGY SAVINGS



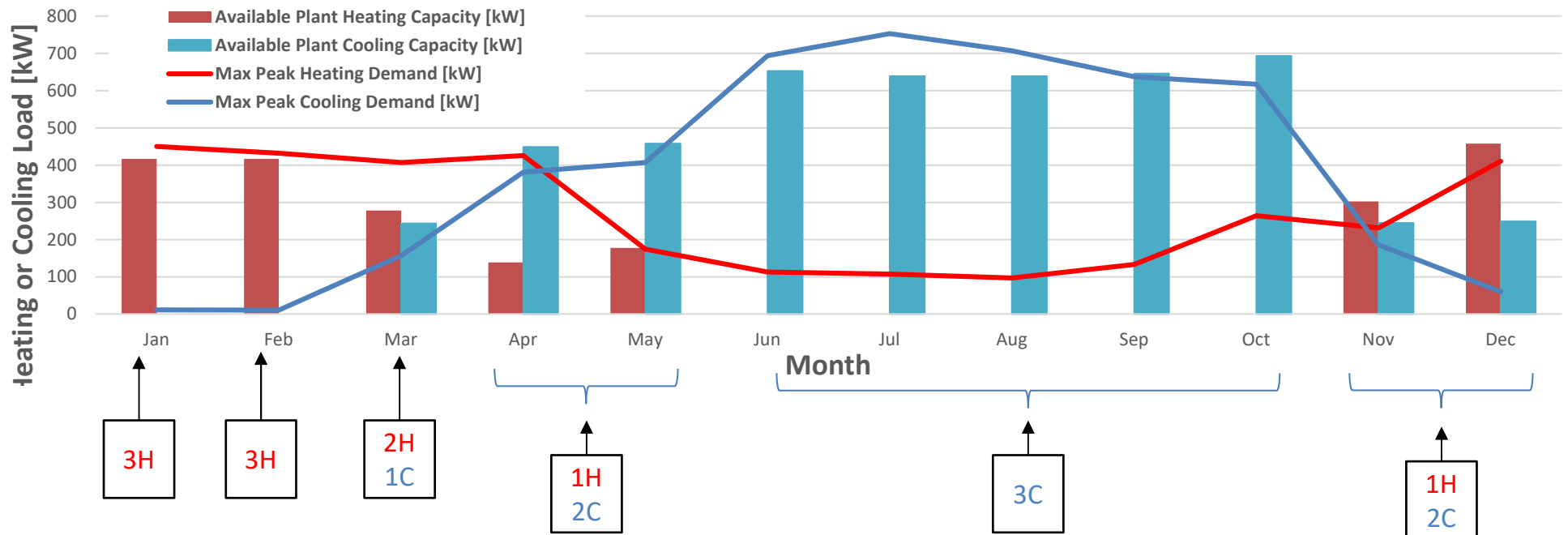
# 2-PIPE AIR-TO-WATER HEAT PUMPS IN 4-PIPE SYSTEMS HEATING & COOLING SIMULTANEOUSLY

## Data Notes:

- Peak Loads shown Reflect Hourly instantaneous peak capacity
- Available Capacities are based on coldest temperature seen during the month for heating, and warmest temperature for cooling
- Where monthly min. Temperature was below  $-10^{\circ}\text{C}$ , available capacity listed is for  $-10^{\circ}\text{C}$

Building Loads are **DYNAMIC**  
So must be the **Heat Pump System!**

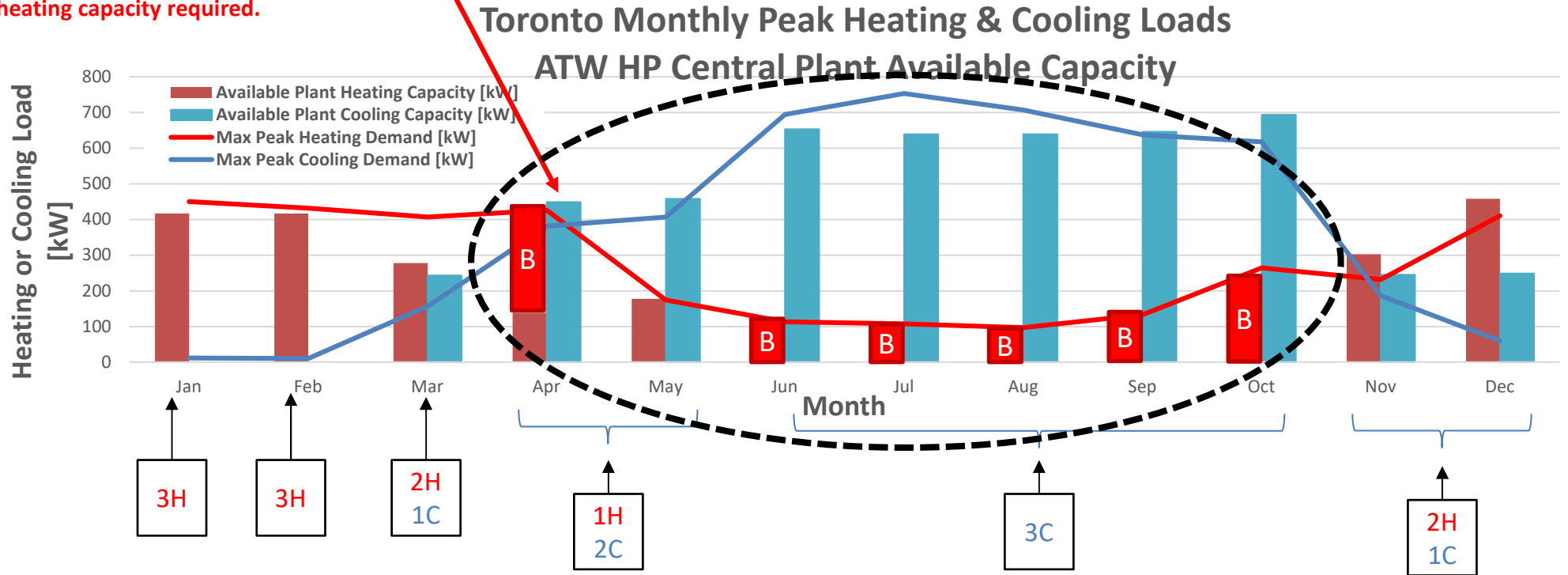
Toronto Monthly Peak Heating & Cooling Loads  
ATW HP Central Plant Available Capacity



# 2-PIPE AIR-TO-WATER HEAT PUMPS IN 4-PIPE SYSTEMS HEATING & COOLING SIMULTANEOUSLY

In cases where equipment can not meet heating and cooling loads at the same time, cooling is prioritized, and the auxiliary boiler makes up the missing heating capacity required.

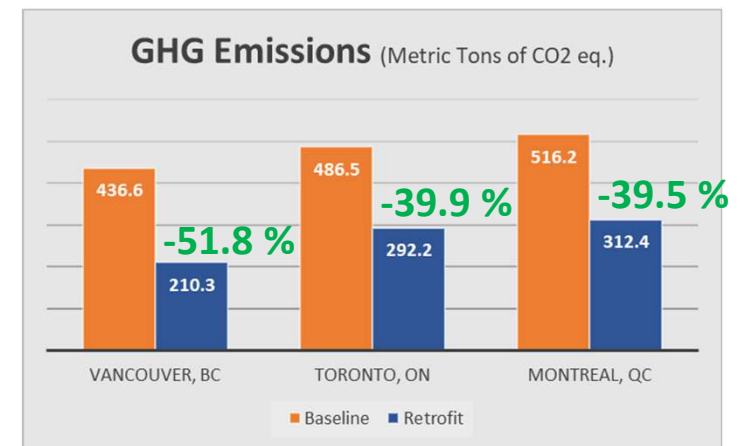
**B** = Load met by Auxiliary Boiler



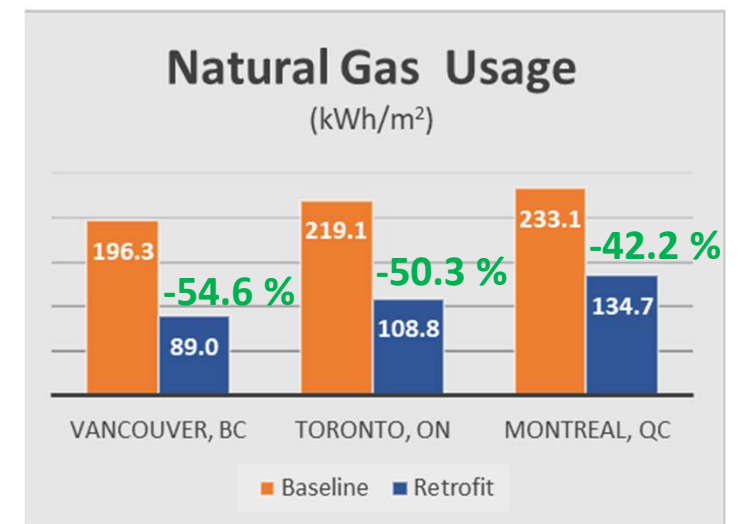
# HYBRID 4-PIPE SYSTEM

## FUEL SWITCH RETROFIT: ENERGY SAVINGS

PRE-RETROFIT			
	<i>Vancouver, BC</i>	<i>Toronto, ON</i>	<i>Montreal, QC</i>
<b>Electric Use Intensity</b> [kWh/m <sup>2</sup> ]	174.0	186.8	186.1
<b>Natural Gas Use Intensity</b> [kWh/m <sup>2</sup> ]	196.3	219.1	233.1
<b>Total EUI</b> [kWh/m <sup>2</sup> ]	370.3	405.9	419.2



POST-RETROFIT			
	<i>Vancouver, BC</i>	<i>Toronto, ON</i>	<i>Montreal, QC</i>
<b>Electric Use Intensity</b> [kWh/m <sup>2</sup> ]	191.3	201.0	197.9
<b>Natural Gas Use Intensity</b> [kWh/m <sup>2</sup> ]	89.0	108.8	134.7
<b>Total EUI</b> [kWh/m <sup>2</sup> ]	280.3	309.8	332.6



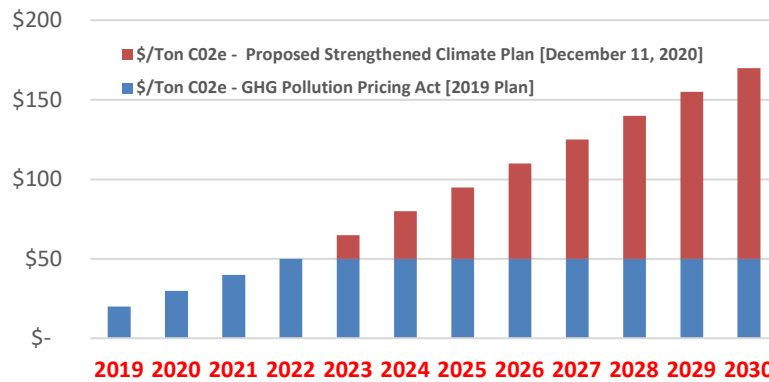


# 2-PIPE AIR-TO-WATER HEAT PUMPS IN 4-PIPE SYSTEMS HEATING & COOLING SIMULTANEOUSLY

Location	Baseline Emissions [Ton CO <sub>2</sub> e]	Retrofit Emissions [Ton CO <sub>2</sub> e]	Annual Tonnes CO <sub>2</sub> e offset
Vancouver	436.6	210.3	<b>226.3</b>
Toronto	486.5	292.2	<b>194.3</b>
Montreal	516.2	312.4	<b>203.8</b>

Simple Payback – ATW HP vs. Like-for-Like Replacement	
Std. Air-Cooled Chiller \$/Ton	\$ 1,200.00
ATW HP \$/Ton	\$ 2,000.00
Incremental Cost, \$/Ton	\$ 800.00
System Sizing (Tons Nominal)	175
<b>Approximate Incremental Cost over like-for-like replacement</b>	<b>\$ 140,328.00</b>

Gov't of Canada Proposed Plan – December 11 2020



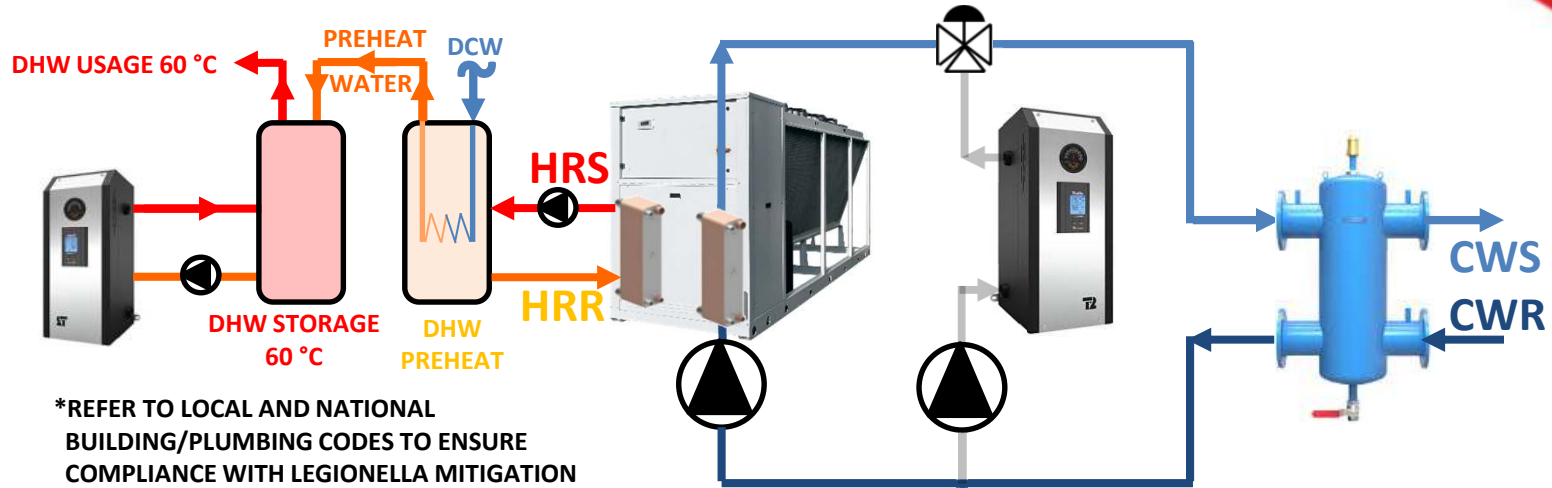
\*\*According to the Plan, if implemented, the Carbon tax will increase by \$15/year until it reaches \$170/ton by 2030

Year	Canadian Federal Carbon Tax* [\$/Ton CO <sub>2</sub> e]	Vancouver		Toronto		Montreal	
		Annual Savings	Cumulative Savings	Annual Savings	Cumulative Savings	Annual Savings	Cumulative Savings
2021	\$ 40	\$ 9,052	\$ 9,052	\$ 7,772	\$ 7,772	\$ 8,152	\$ 8,152
2022	\$ 50	\$ 11,315	\$ 20,367	\$ 9,715	\$ 17,487	\$ 10,190	\$ 18,342
2023	\$ 65	\$ 14,710	\$ 35,077	\$ 12,630	\$ 30,117	\$ 13,247	\$ 31,589
2024	\$ 80	\$ 18,104	\$ 53,181	\$ 15,544	\$ 45,661	\$ 16,304	\$ 47,893
2025	\$ 95	\$ 21,499	\$ 74,679	\$ 18,459	\$ 64,119	\$ 19,361	\$ 67,254
2026	\$ 110	\$ 24,893	\$ 99,572	\$ 21,373	\$ 85,492	\$ 22,418	\$ 89,672
2027	\$ 125	\$ 28,288	\$ 127,860	\$ 24,288	\$ 109,780	\$ 25,475	\$ 115,147
2028	\$ 140	\$ 31,682	\$ 159,542	\$ 27,202	\$ 136,982	\$ 28,532	\$ 143,679
2029	\$ 155	\$ 35,077	\$ 194,618	\$ 30,117	\$ 167,098	\$ 31,589	\$ 175,268
2030	\$ 170	\$ 38,471	\$ 233,089	\$ 33,031	\$ 200,129	\$ 34,646	\$ 209,914

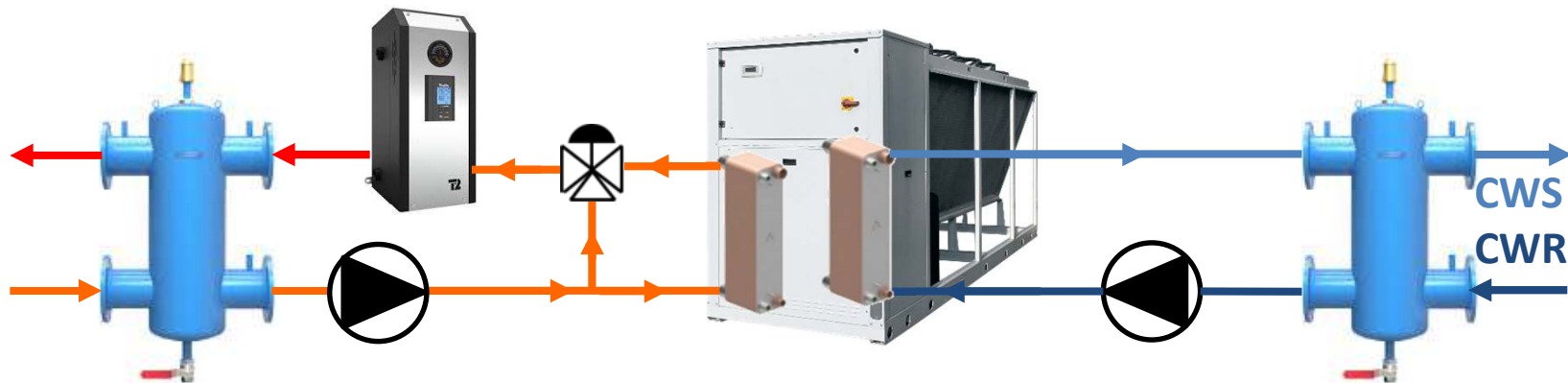
\$/Ton CO<sub>2</sub>e Federal Carbon Charge

# PARTIAL HEAT RECOVERY USING DESUPERHEATER

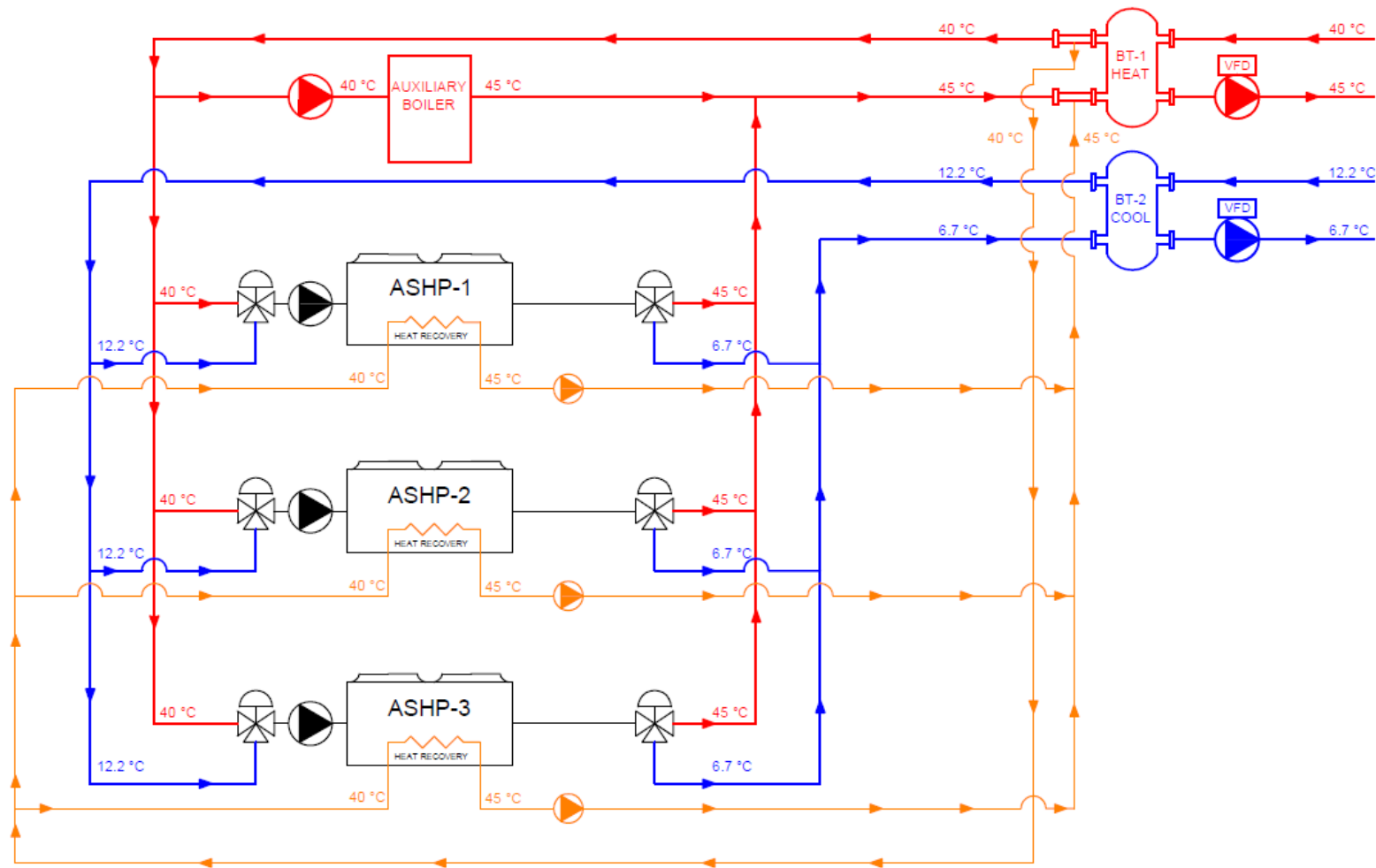
HEAT RECOVERY TO DOMESTIC HOT WATER SYSTEM (2-PIPE SYSTEM)



HEAT RECOVERY TO BOILER PRE-HEAT (4-PIPE SYSTEM)



# PARTIAL HEAT RECOVERY USING DESUPERHEATER 4-PIPE SYSTEMS



# SUMMARY

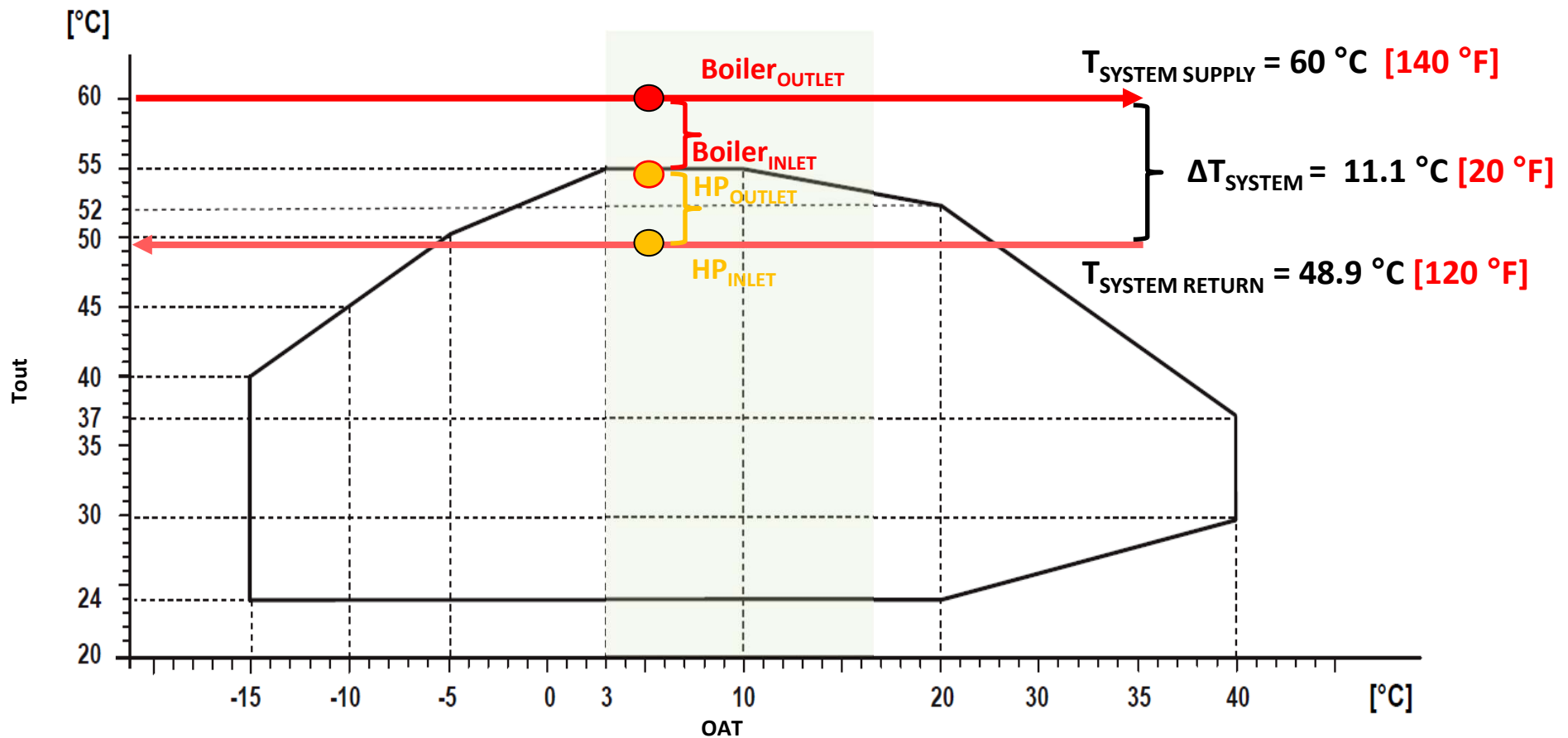
- **HOLISTIC APPROACH TO MECHANICAL DESIGN IS REQUIRED TO MEET GHG REDUCTION TARGETS**
  - “ONE-SIZE-FITS-ALL” IS NOT ALWAYS COMPATIBLE WITH LOW CARBON
  - SIGNIFICANT SAVINGS CAN BE ACHIEVED WHILE USING CURRENT ATW TECHNOLOGY WITHIN LIMITATIONS
  - REDUCED OPERATING TEMP = INCREASED EFFICIENCY + FACILITATED INTEGRATION
- **INCORPORATING OTHER MEASURES (ENVELOPE UPGRADE) ARE EQUALLY IMPORTANT**
  - LESS HEAT LOSS = REDUCED RETROFIT EQUIPMENT SIZING
  - REDUCED POWER REQUIREMENT FOR ELECTRIFIED HEATING RETROFITS
- **DUAL FUEL PROVIDES BUILDING RESILIENCY**
  - LEVERAGE EXISTING NATURAL GAS INFRASTRUCTURE WHERE IT MAKES SENSE
  - FLEXIBILITY TO MANAGE CARBON FOOTPRINT OR OPERATING COST VIA ENERGY MANAGEMENT STRATEGY
  - TRANSITION TO LOWER EMISSION NATURAL GAS WITH RNG OVER TIME
  - FUTURE PROOFED BUILDING: ATW HP TECHNOLOGY IMPROVEMENT AT END OF LIFECYCLE
  - ELECTRICAL GRID CAPACITY MANAGEMENT
- **TRANSFORMATION OF FINANCIAL/BUSINESS CASE TO SUPPORT LOW-CARBON TRANSITION**
  - OPERATING OR FIRST COST IS NO LONGER THE GOVERNING CRITERIA
  - RETROFIT CODE & TARGETS WILL ACCELERATE ADOPTION
  - FINANCIAL SUPPORT FOR PRIVATE SECTOR + FUEL SWITCHING PROJECT SUPPORT WILL LAUNCH ATW INTO MAINSTREAM



**QUESTIONS?**

# DESIGN CONSIDERATION: AUXILIARY HEAT

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